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► **To cite this version:**

I. Gaballah, Silvester Ivanaj, Ndue Kanari. Kinetics of chlorination and oxychlorination of chromium (III) oxide. Metallurgical and Materials Transactions A, Springer Verlag/ASM International, 1998, 29 (4), pp. 1299-1308. <10.1007/s11661-998-0256-1>. <hal-01508117>

HAL Id: hal-01508117

<https://hal.univ-lorraine.fr/hal-01508117>

Submitted on 5 May 2017

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Kinetics of Chlorination and Oxychlorination of Chromium (III) Oxide

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Thermogravimetric analysis (TGA) is used to study the kinetics of chlorination of Cr₂O₃ with Cl₂+N₂ and Cl₂+O₂ gas mixtures in the temperature range of 550 °C to 1 000 °C. The reactivity of Cr₂O₃ towards chlorine-oxygen gas mixture is higher than that of chlorine-nitrogen one.

Chlorination of Cr₂O₃ proceeds with an apparent activation energy of about 86 kJ/mol between 550 °C and 1 000 °C. The apparent reaction order with respect to chlorine is about 1.23 at 800 °C. At temperatures lower than 650 °C, the shrinking sphere model is the most appropriate for describing the reaction kinetics^[19].

Oxychlorination of Cr₂O₃ is characterized by an apparent activation energy of about 87 and 46 kJ/mol for temperatures lower than 650 °C and higher than 700 °C, respectively. At 800 °C and using a Cl₂+O₂ gas mixture, the maximum reaction rate is obtained by using a gas mixture having a Cl₂/O₂ molar ratio equal to 4 confirming the formation of chromium oxychloride. At this temperature, the reaction order with respect to chlorine, oxygen and Cl₂+O₂ is about 1.08, 0.23 and 1.29, respectively. All the experimental data match with the general kinetic equation : $kt = 1-(1-X)^{1/F(p)} = kt$ ^[19]. Only, the value of the particle shape factor, 'F_(p)', is different.

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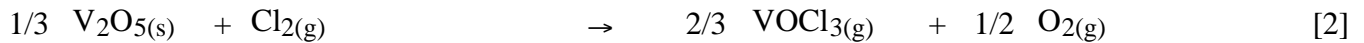
I. INTRODUCTION AND LITERATURE REVIEW

Reactivity of chlorine towards metals and metal compounds is interesting for the recovery of a valuable element from their ores and/or from industrial wastes. The chlorides and oxychlorides of transition metals have, generally, a lower boiling points than their oxides. This may allow selective separation of one or several elements, from the gas phase, by controlled cooling of reaction products. Recently, chlorination was used for the recovery of Ta and Nb from their ores^[1] and tin slag^[2] as well as for the extraction of Mo and V from spent hydrorefining catalysts^[3,4]. Chlorination is also investigated for the beneficiation of chromite concentrates and/or selective separation of chromium compounds^[5,6].

This paper is devoted to the study of the chlorination and the oxychlorination kinetics of chromium (III) oxide using Cl_2+N_2 and Cl_2+O_2 gas mixtures. This investigation is a part of a larger program concerning the chlorination of refractory metals such as MoO_3 ^[7], V_2O_5 ^[8], Nb_2O_5 and Ta_2O_5 ^[9]. Moreover, the generated data could be used for the beneficiation of chromite ores or concentrates and for the recovery of chromium compounds from industrial wastes.

Chlorination of Mo, V, Nb and Ta oxides, without a reducing agent, generates oxychlorides of these elements. The most common oxychlorides are those described by Eqs 1 to 4. These reactions indicate that a half mole of oxygen is evolved because it substituted by a chlorine mole without changing the element valency. The most probable oxychloride of chromium is $\text{CrO}_2\text{Cl}_{2(\text{g})}$ ^[10]. For this reason, the formation of $\text{CrO}_2\text{Cl}_{2(\text{g})}$ through the chlorination of Cr_2O_3 required extra oxygen as shown by Eq 5.

The literature is relatively poor concerning the Cr-O-Cl system. The reaction products of chromium (III) oxide with chlorine could be CrCl_2 , CrCl_3 , CrCl_4 and CrO_2Cl_2 depending on the temperature and Cl_2 and O_2 partial pressures of the system. Morozov and Fefelova^[11] studied the equilibrium of chlorination of Cr_2O_3 with Cl_2 between 700 °C and 1000 °C. They mentioned that the chlorination of chromium (III) oxide by chlorine at high temperature could lead to the formation of CrCl_2 , CrCl_3 and CrCl_4 . These authors suggested that the formation of chromium oxychlorides, in the investigated temperature range, is almost improbable because of their instability at temperatures higher than 450 °C. Sano and Belton^[12] have a thermodynamic approach for the formation of $\text{CrO}_2\text{Cl}_{2(\text{g})}$ using the transpiration method. Their experiments consist on the measurement of the volatilization of chromic oxide in a $\text{Cl}_2+\text{O}_2+\text{Ar}$ atmosphere. According to these authors, the $\text{CrO}_2\text{Cl}_{2(\text{g})}$ is the chromium predominant product of Cr_2O_3 reaction with Cl_2+O_2 between 627 °C to 977 °C and the reaction is that described by Eq 5. Reinhold and Hauffe^[13] studied the chlorination kinetics of chromium metal and Cr_2O_3 pellets by thermogravimetric analysis (TGA). They concluded that the rate constant of Cr_2O_3 reaction with Cl_2+O_2 increases linearly with Cl_2 pressure and with fourth root of the O_2 pressure indicating that $\text{CrO}_2\text{Cl}_{2(\text{g})}$ could be the only reaction product. The investigation of Plies^[14] by mass spectrometric reveals the presence $\text{CrOCl}_{2(\text{g})}$ in the gas phase of the system $\text{CrOCl}-\text{Cl}_2$ and $\text{Cr}_2\text{O}_3-\text{Cl}_2$ between 627 °C and 1077 °C.



The formation of $\text{CrO}_2\text{Cl}_2(\text{g})$, during the oxychlorination of Cr_2O_3 -forming alloys with $\text{Cl}_2+\text{O}_2+\text{Ar}$, is also confirmed by Jacobson et al.^[15] using mass spectrometric and TG techniques. In another paper, McNallan et al.^[16] used the same techniques in attempt to test the corrosion of Ni-Cr alloys in flowing $\text{Cl}_2+\text{O}_2+\text{Ar}$ gas mixtures. They mentioned that the principal volatile corrosion products are $\text{NiCl}_2(\text{g})$ and $\text{CrO}_2\text{Cl}_2(\text{g})$.

II. THERMODYNAMIC STUDY

Equations 5 and 7 to 10 were considered to describe the possible chemical reactions of Cr_2O_3 with Cl_2+O_2 and Cl_2 gas mixtures up to 1000 °C. The formation of CrCl_2 is neglected due to high oxidation ability of chlorine. The chromium oxychloride is presumed as the only product of reaction of Cr_2O_3 with Cl_2+O_2 (Eq 5). The evolution of the standard free energy changes (ΔG°) of these reactions, as a function of temperature, is shown in Figure 1. The thermodynamic data, used in this study, are those of Barin^[17]. This figure shows that the standard free energy changes of all the reactions are positive. However, an important criterion for determining the thermodynamic possibility of a chemical reaction is the evaluation of its free energy change (ΔG) given by :

$$\Delta G = \Delta G^\circ + RT \ln K \quad [6]$$

Although the reaction described by equation 5 at 800 °C is characterized by ΔG° of about 20 kJ/mol, the value of equilibrium constant for $\Delta G = 0$ is about 0.106. This value indicates that the formation of $\text{CrO}_2\text{Cl}_2(\text{g})$ is possible at this temperature specially that the partial pressure of this compound in the gas phase is very low. This enhances the oxychlorination rate of Cr_2O_3 .



III. MATERIALS AND EXPERIMENTAL PROCEDURE

The sample used in this study is a Cr_2O_3 powder supplied by LABORATOIRES STANDA having a purity higher than 99 %. The sample's spectra of X-rays diffraction (XRD) and that obtained by the electron probe microanalysis of the scanning electron microscope (EPMA-SEM) indicate the presence of only Cr_2O_3 phase. The specific surface area of the sample was about $3.8 \text{ m}^2/\text{g}$.

The chlorination kinetics of Cr_2O_3 was determined by thermogravimetric analysis technique described previously.^[8] The experimental tests were carried out in non and isothermal conditions. A sample of about 40 mg, placed in a large boat, is used for each test. For TG tests in non isothermal conditions, the sample was directly heated in the chlorinating gas atmosphere. The furnace heating rate was kept at about $7 \text{ }^\circ\text{C}/\text{minute}$. For isothermal runs, the sample was heated in nitrogen atmosphere to a given temperature before the introduction of the chlorinating gas mixture. The exhaust gases were neutralized by NaOH before their release to the atmosphere.

IV. RESULTS

A. Non Isothermal Treatment of Cr_2O_3 and CrCl_3 in Cl_2+N_2 and Cl_2+O_2 Gas Mixtures

Non isothermal TG measurements were performed up to $1000 \text{ }^\circ\text{C}$ to compare the reactivity of Cr_2O_3 towards Cl_2+N_2 and Cl_2+O_2 atmospheres. Figure 2 shows the evolution of the percent weight loss of chromium (III) oxide *versus* temperature during its chlorination and oxychlorination. This figure also includes the volatilization and/or reaction curves of CrCl_3 using the same chlorinating atmosphere.

The data analysis indicates that Cr_2O_3 starts to react with the two gas mixtures at temperature higher than $550 \text{ }^\circ\text{C}$. However, the chlorination rate augments with increasing the oxygen partial pressure in the gas mixture. At $1000 \text{ }^\circ\text{C}$, the reaction extent of Cr_2O_3 with Cl_2+O_2 and Cl_2+N_2 was about 100 and 70 pct, respectively. The rate of volatilization and/or reaction of CrCl_3 with the chlorinating gas mixtures depends on the oxygen partial pressure. Chromium trichloride starts to volatilize and/or to react with the reactive gases at about $475 \text{ }^\circ\text{C}$. The curve of pct weight loss of CrCl_3 in Cl_2+O_2 undergoes an anomaly at about $630 \text{ }^\circ\text{C}$. The SEM and XRD analysis of residue obtained at this temperature indicate the presence of Cr_2O_3 . This is probably due to the oxidation of CrCl_3 according to equation 7 and in spite of the important chlorine partial pressure.

It is important to underline that the reaction and/or volatilization rate of CrCl_3 in Cl_2+N_2 is largely higher than the chlorination rate of Cr_2O_3 with this gas mixture. Thus, during Cr_2O_3 chlorination, the reaction rate can be evaluated by the weight loss of sample in the chlorinating atmosphere. On the other hand, the product of Cr_2O_3 oxychlorination ($\text{CrO}_2\text{Cl}_2(\text{g})$) is very volatile in the temperature range explored as its boiling point is about 117°C [10,18].

B. Kinetics of Chlorination of Cr_2O_3 by Cl_2+N_2

1. Effect of gas flow rate

The effect of Cl_2+N_2 flow rate on the reaction rate is performed to determine the conditions where the external mass transfer phenomena could be minimized. A series of isothermal tests is carried out at 950°C using a total gas flow rate that varies from 8 to 72 L/h while keeping the Cl_2/N_2 molar ratio equal to 1. Figure 3 illustrates the evolution of reaction rate as a function of gas velocity ' V_g ' for a reaction extent X (weight ratio of reacted fraction to the initial sample) of 0.05 to 0.4. It is clear that the reaction rate is independent for a gas velocity higher than 33 cm/min. A gas flow rate of 60 L/h ($V_g \approx 50$ cm/min) is used during the study of the chlorination kinetics of Cr_2O_3 with Cl_2+N_2 .

2. Effect of temperature

The effect of temperature on the chlorination of Cr_2O_3 with Cl_2+N_2 ($\text{Cl}_2/\text{N}_2 = 1$) is studied between 550°C and 1000°C . Figure 4 illustrates the evolution of pct weight loss of the sample *versus* time. The reaction rate augments steadily with the temperature increase. The temperature coefficient of the reaction rate is shown in Figure 5. Between 550°C and 1000°C , the apparent activation energy ' E_a ' of the chlorination of chromium oxide is 86 ± 2 kJ/mol.

Different kinetics' equations are tried to correlate the experimental data with these asymptotic equations. The following equations (Eqs 11 to 14) could be used to describe the evolution of reaction extent as a function of time for this gas-solid reaction. They are deduced from those described by Szekely et al. [19]

$$1-(1-X)^{1/F_p} = kt \quad [11]$$

$$X = kt \quad (\text{for } F_p = 1) \quad [12]$$

$$1-(1-X)^{1/2} = kt \quad (\text{for } F_p = 2) \quad [13]$$

$$1-(1-X)^{1/3} = kt \quad (\text{for } F_p = 3) \quad [14]$$

where X = extent of reaction,

F_p = particle shape factor (1 for infinite slabs, 2 for long cylinders, and 3 for spheres),

k = constant and t = chlorination time.

Equation 10 describes a reaction controlled by the chemical reaction in shrinking nonporous particles (with or without a solid porous product) and porous particles with unchanged overall sizes. It also applies for pore diffusion control in the case of complete gasification of porous solids.

The best mathematical fitting of the experimental data of Figure 4 (a) is obtained using Eq 14 ($0.0 \leq X \leq 0.8$) as illustrated by Figure 6 (a). The average correlation coefficient is about 0.998. Between 800 °C and 1000 °C, the best fitting of experimental data is obtained using Eq 12 with a correlation coefficient higher than 0.999 as shown in Figure 6 (b). The evolution of the particle shape factor for experimental data is shown in Figure 6 (c).

At temperatures lower than 700 °C, the value of F_p is about 3 describing the classical shrinking sphere model where the reaction product is a gas and the grain particles of chromium oxide decrease as the reaction extent increases. At temperatures higher than 800 °C, the shape factor is about 1 that may indicate that the chlorination rate of Cr_2O_3 is controlled by external mass transfer. This is in contradiction with the data of Figure 3. It seems that the reaction path changes at about 750 °C. Figure 1 shows that the reaction products could be either CrCl_3 or CrCl_4 at temperatures lower and higher than 750 °C, respectively. This may explain the change of the value of the shape factor in the temperature range of 700 °C to 800 °C although no direct experimental measurements are available.

3. Apparent reaction order with respect to Cl_2

To determine the effect of Cl_2 partial pressure on the reaction rate, a series of isotherms is performed at 800 °C using a Cl_2+N_2 gas mixture with a gas velocity of 50 cm/min. The chlorine partial pressure was varied from 0.10 to 1.00 atm. The weight loss evolution *versus* time for each isotherm is shown in Figure 7 (a). The mathematical fitting of this figure's data is plotted in Figure 7 (b) for X as a function of time. The average correlation coefficient is about 0.999. This indicates that the chlorination mechanism of Cr_2O_3 is the same within a chlorine partial pressure of 0.1 to 1 atm. The slope of curve of Figure 8 indicates that the reaction order with respect to Cl_2 ' n_{Cl_2} ' is 1.23 ± 0.04 .

C. Kinetics of Oxychlorination of Cr_2O_3 by Cl_2+O_2 .

1. Effect of gas flow rate

This effect was studied at 1000 °C using a gas mixture containing Cl_2+O_2 ($\text{Cl}_2/\text{O}_2 = 4$) during the oxychlorination of chromium oxide. The evolution of reaction rate as a function of gas velocity is illustrated in Figure 9. The reaction rate is independent from the gas flow rate for a linear velocity of the reactive gases higher than 24.8 cm/min. For this reason, a gas flow rate having $V_g = 33$ cm/min (40 L/h) is used for further experiments on oxychlorination of Cr_2O_3 .

2. Effect of $\text{Cl}_2/(\text{Cl}_2+\text{O}_2)$ ratio

To get an insight of the oxychlorination mechanism of Cr_2O_3 , a series of experiments is carried out at 800 °C with $\text{Cl}_2/(\text{Cl}_2+\text{O}_2)$ molar ratio varying from 0 to 1.0. The gas velocity was kept constant and equal to 33 cm/min. Figure 10 shows the evolution of the reaction rate versus $\text{Cl}_2/(\text{Cl}_2+\text{O}_2)$ molar ratio. The oxychlorination rate passes by a maximum corresponding to a $\text{Cl}_2/(\text{Cl}_2+\text{O}_2)$ molar ratio at about 0.8. This value corresponds to a molar ratio of Cl_2/O_2 equal to 4. These results show that the chlorination of chromium (III) oxide with Cl_2+O_2 mixture takes place according to reaction 5 involving the formation of $\text{CrO}_2\text{Cl}_2(\text{g})$ as the main reaction product.

In an attempt to confirm the $\text{CrO}_2\text{Cl}_2(\text{g})$ formation, a few experiments were performed with 2 grams of Cr_2O_3 sample between 800 °C and 1000 °C for a reaction time of 2 hours. The experiments are carried out using a horizontal set^[20] and a gas mixture having Cl_2/O_2 molar ratio equal to 4. The exhaust gases were successively cooled at 25 °C and -35 °C. No solid condensate is observed by cooling the exhaust gases at 25 °C indicating the absence of chromium chlorides' formation. However, cooling the vapor phase to - 35 °C leads to the formation of a red liquid. This liquid decomposes in air and explodes with alcohol. The qualitative chemical analysis indicates that the solid generated by the decomposition of this liquid is essentially chromium oxide. The properties of the obtained red liquid are in good agreement with those reported by reference [10] for the $\text{CrO}_2\text{Cl}_2(\text{g})$.

3. Apparent reaction order with respect to Cl_2+O_2

The experiments for determining the apparent reaction order with respect to Cl_2+O_2 were performed at 800 °C. The Cl_2/O_2 molar ratio is kept constant and equal to 4 in the gas mixture, while the partial pressure of Cl_2+O_2 is varied from 0.38 to 1.00 atm by diluting the gas mixture with nitrogen. The evolution of the reaction rate as a function of Cl_2+O_2 partial pressure is shown by Figure 11. The apparent reaction order ' $n_{(\text{Cl}_2+\text{O}_2)}$ ' deduced from these data is 1.29 ± 0.01 .

4. Apparent reaction orders with respect to Cl₂ and to O₂

The effect of Cl₂ and O₂ partial pressure is examined at 800 °C. Two series of tests were carried out using Cl₂+O₂+N₂ with a flow rate of 33 cm/min. The first series of tests is performed by keeping the oxygen partial pressure constant (0.33 atm) and varying the chlorine partial pressure from 0.14 to 0.52 atm. The second one is conducted using a constant chlorine partial pressure (0.33 atm) and varying the oxygen partial pressure from 0.14 to 0.52 atm.

Figures 12 and 13 trace the evolution of natural logarithm of reaction rates as a function of that of chlorine and oxygen partial pressures, respectively. The apparent reaction orders with respect to chlorine ' n_{Cl_2} ' and to oxygen ' n_{O_2} ' are obtained by the linearization of data of these figures. The value of ' n_{Cl_2} ' and ' n_{O_2} ' are 1.08 ± 0.02 and 0.23 ± 0.01 , respectively. This confirms that the presence of oxygen enhances the reaction rate. This observation confirms the formation of CrO₂Cl₂(g) as described by Eq 5. On the other hand, one may underline that the global reaction order is almost equal to the algebraic sum of the partial ones, i.e., $n_{(Cl_2+O_2)} \approx n_{Cl_2} + n_{O_2}$.

5. Effect of temperature

This effect on the oxychlorination of chromium (III) oxide is investigated by isothermal measurements between 540 °C and 1000 °C. A Cl₂+O₂ (Cl₂/O₂ = 4) gas mixture having a total flow rate of 33 cm/min is used. The evolution of the sample's pct weight loss *versus* time for different temperatures is shown in Figures 14 (a) and (b). At 550 °C, about 45 pct of the sample is chlorinated for a reaction time of 500 minutes while at 950 °C only 25 minutes are necessary to attain the same reaction extent. The Arrhenius plot of oxychlorination of Cr₂O₃ is traced in Figure 15 and presents a classical evolution of a solid-gas reaction kinetics as a function of temperature.^[19] The apparent activation energy changes from 87 kJ/mol, below 650 °C, to 46 kJ/mol for temperatures higher than 700 °C.

Figure 16 illustrates the evolution of specific surface area of partially oxychlorinated samples ($X \approx 0.27$) of Cr₂O₃ as a function of temperature. The samples' specific surface area decreases sharply for temperatures higher than 600 °C and this phenomenon could be related to the decrease of E_a that occurs at about 650 °C.

Mathematical fitting of the experimental data of Figure 14 is examined using Eqs 11 to 14. The plots of the best fitting are represented in Figures 17 (a) and (b). At temperatures lower than 650 °C, equation

14 applies to the experimental data with an average correlation coefficient of 0.998 (Fig. 17 a). The values of apparent activation energy coupled with this equation indicate that the rate-controlling step of overall process could be the chemical reaction. The data of experiments carried out between 700 °C and 1000 °C are linearized by using Eq 13 giving $1-(1-X)^{1/2}$ versus time (Fig. 17 b) with a correlation coefficient higher than 0.999. At temperatures higher than 700 °C, the decrease of the specific surface area could be related to the modification of shape factor of grains and to the decrease of the value of the apparent activation energy.

Figures 18 (a), (b) and (c) summarize plots of Eq 13 of the data obtained during the oxychlorination of Cr_2O_3 at 800 °C for various partial pressures of Cl_2+O_2 , Cl_2 and O_2 , respectively. The average correlation coefficient of data linearization for $0 \leq X \leq 0.8$ is higher than 0.999. It can be concluded that the reaction mechanism is not affected by the change of the partial pressures of reactive gases in the pressure range investigated at 800 °C.

The effect of temperature on the chlorination and oxychlorination of chromium (III) oxide is compared in Figure 19. At 500 °C, the reactivity of Cr_2O_3 towards Cl_2+N_2 is low and the reaction rate is about 0.01 pct weight loss per minute. On the other hand, the oxychlorination rate of Cr_2O_3 is higher than that of its chlorination specially at low temperatures.

The oxychlorination of the chromium oxide bearing materials with Cl_2+O_2 ($\text{Cl}_2/\text{O}_2 = 4$) at temperatures higher than 800 °C could be suggested for the separation of chromium compounds from these solids.

V. CONCLUSIONS

Analysis of the thermodynamic data of the possible chlorination reactions of chromium oxide shows that the most probable reaction product of Cr_2O_3 chlorination is chromium(VI) oxychloride.

The reaction of Cr_2O_3 with a Cl_2+N_2 and Cl_2+O_2 gas mixture starts at temperatures higher than 550 °C. The reactivity of chromium oxide towards the oxychlorinating gas mixture is higher than that of the chlorinating gas mixture. The rate of volatilization and/or reaction of chromium trichloride, with the two chlorinating gas mixtures, is higher than that of its generation during the chlorination of chromium (III)

oxide and justifies the use of TGA to study the chlorination kinetics of Cr_2O_3 .

At 800 °C, the apparent reaction order with respect to chlorine is about 1.23. Between 550 °C and 1 000 °C, the chlorination of Cr_2O_3 by Cl_2+N_2 proceeds with an apparent activation energy of 86 kJ/mol. Mathematical fitting of the experimental data suggests that the reaction bath changes at about 650 °C. At temperatures lower than 650 °C, the shrinking sphere model is the most appropriate for describing the reaction's kinetics.

The apparent activation energy of Cr_2O_3 oxychlorination is about 87 kJ/mol at temperatures lower than 650 °C and decreases to 46 kJ/mol for temperatures higher than 700 °C. The mathematical modeling of the experimental data obtained during the oxychlorination of chromium oxide indicates a change of the shape factor from 3 to 2 around 650 °C. These results could be attributed to the sharp decrease of the specific surface area of the Cr_2O_3 sample, at about 600 °C, during its oxychlorination.

The oxychlorination reaction rate of Cr_2O_3 by Cl_2+O_2 passes by a maximum for a gas mixture having a molar ratio of Cl_2/O_2 equal to 4. The reaction order with respect to chlorine, oxygen and Cl_2+O_2 is 1.08, 0.23 and 1.29, respectively. The overall reaction order is almost equal to the algebraic sum of the fractional ones. These results confirm the formation of chromium oxychloride as the final reaction's product of Cr_2O_3 oxychlorination. Data analysis indicates that the reaction mechanism is independent of the composition of the oxychlorinating gas mixture in the explored range.

These results suggest that the separation of chromium compounds from chromium bearing materials is possible using an oxychlorinating gas mixture at temperatures equal or higher than 800 °C.

ACKNOWLEDGMENTS

This work was performed in the frame of contract N° BRE2-CT92-0173 thanks to the financial support of the European Union (DG-XII). The authors thank Drs. H. L. Schmidt for discussion, suggestion and help.

They also would like to thank Drs. J. C. Mugica (INASMET, San Sebastian, Spain) and M. Coelho (INETI, Lisbon, Portugal) for technical discussions. Authors are indebted to A. Bonazébi, M. Djona, N. Menad and N. Mirghaffari for discussions and help on different subjects and to Mrs. C. Tanchel for technical and administrative support.

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FIGURE CAPTIONS

- Figure 1 : Standard free energy change of Cr_2O_3 chlorination reactions as a function of temperature.
- Figure 2 : TG analysis of Cr_2O_3 and CrCl_3 treatment in Cl_2+N_2 and Cl_2+O_2 .
- Figure 3 : Chlorination rate of Cr_2O_3 as a function of flow rate of the Cl_2+N_2 mixture.
- Figure 4 : Isotherms of chlorination of Cr_2O_3 with Cl_2+N_2 for (a) $T \leq 775$ °C and (b) $T \geq 800$ °C.
- Figure 5 : Arrhenius plot of chlorination of Cr_2O_3 by Cl_2+N_2 .
- Figure 6 : Mathematical fitting of the chlorination data at (a) $T \leq 700$ °C using Eq. 14 and (b) $T \geq 800$ °C using Eq. 12.
- Figure 7 : Isotherms of chlorination of Cr_2O_3 (a) using different chlorine pressures and (b) linearization of data using Equation 12.
- Figure 8 : Apparent reaction order of Cr_2O_3 chlorination with respect to chlorine.
- Figure 9 : Chlorination rate of Cr_2O_3 as a function of flow rate of the Cl_2+O_2 mixture.
- Figure 10 : Effect of $\text{Cl}_2/(\text{Cl}_2+\text{O}_2)$ molar ratio on the reaction rate of Cr_2O_3 oxychlorination.
- Figure 11 : Apparent reaction order with respect to Cl_2+O_2 .
- Figure 12 : Apparent reaction order with respect to Cl_2 .
- Figure 13 : Apparent reaction order with respect to O_2 .
- Figure 14 : Isotherms of chlorination of Cr_2O_3 with Cl_2+O_2 for (a) $T \leq 700$ and (b) $T \geq 750$ °C.
- Figure 15 : Arrhenius plot of chlorination of Cr_2O_3 by Cl_2+O_2 .
- Figure 16 : Evolution of the specific surface area of partially oxychlorinated samples ($X \approx 0.27$) of Cr_2O_3 as a function of temperature.
- Figure 17 : Mathematical fitting of the oxychlorination data at (a) $T \leq 650$ °C and (b) $T \geq 700$ °C using Eqs 14 and 13, respectively.
- Figure 18 : Mathematical fitting of the oxychlorination data at 800 °C using Eq 13
(a) for different (Cl_2+O_2) partial pressure, (b) for different Cl_2 partial pressure and
(c) for different O_2 partial pressure.
- Figure 19 : Comparison of Arrhenius plots of chlorination and oxychlorination of Cr_2O_3 .

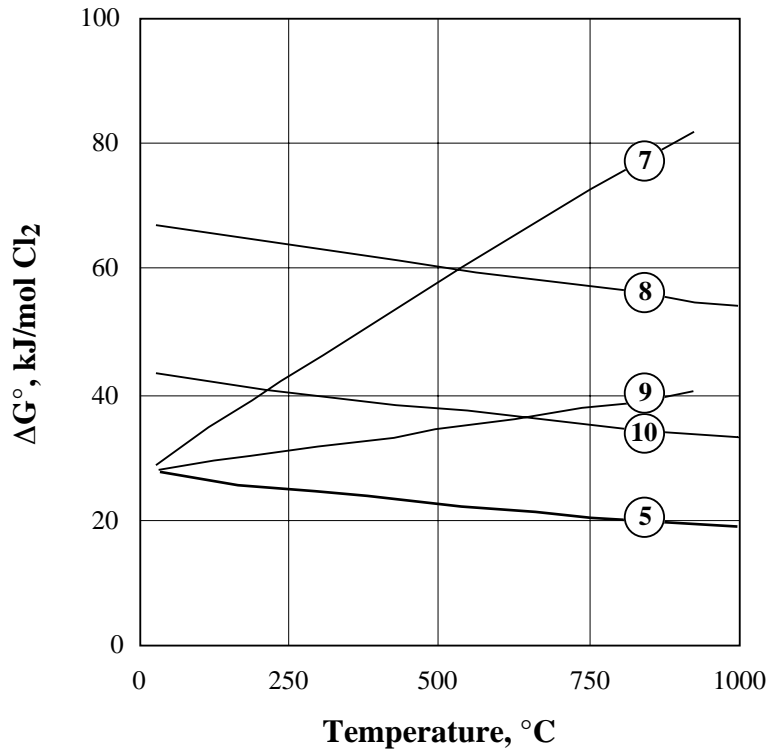


Fig. 1- Standard free energy changes of Cr_2O_3 chlorination reactions as a function of temperature.

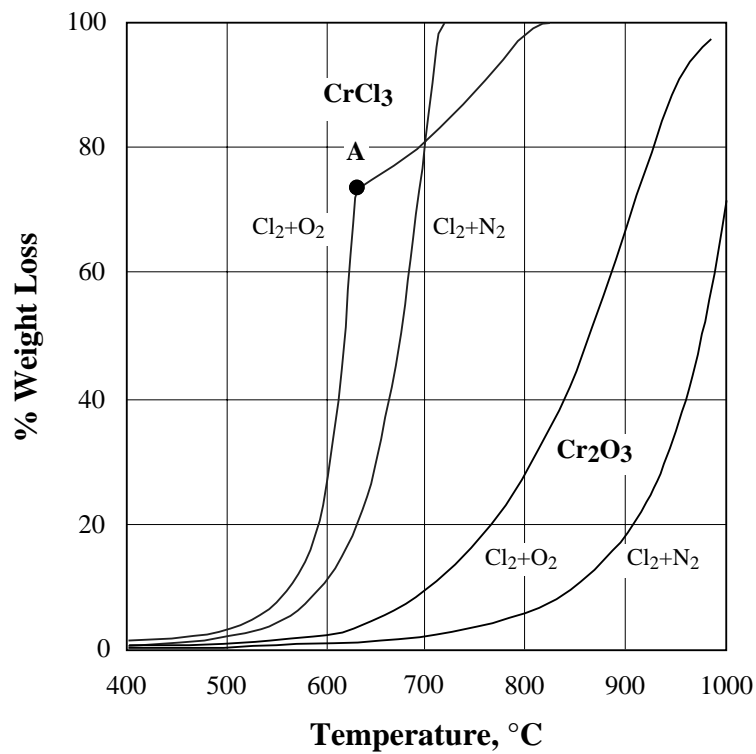


Fig. 2- TG analysis of Cr_2O_3 and CrCl_3 treatment in Cl_2+N_2 and Cl_2+O_2 .

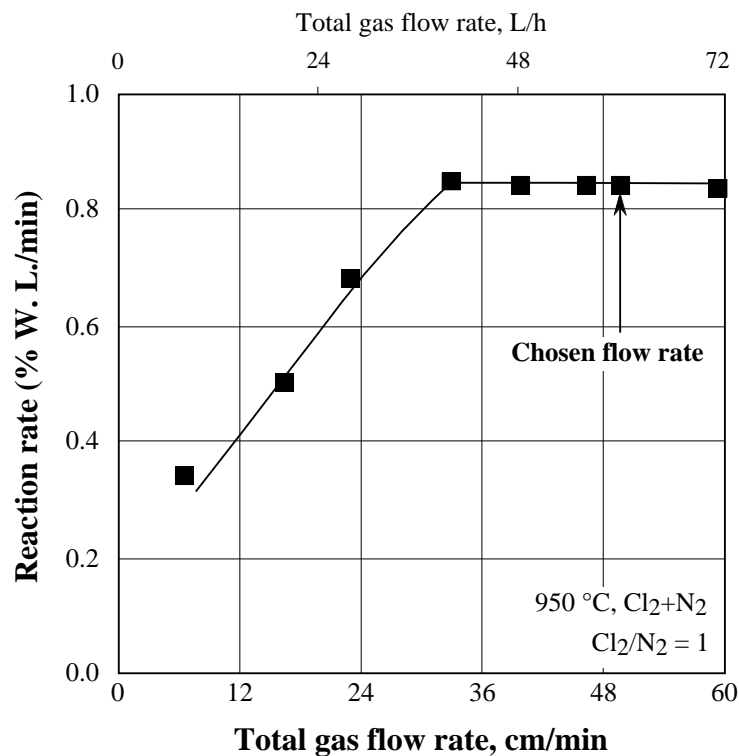


Fig. 3- Chlorination rate of Cr_2O_3 as a function of flow rate of the Cl_2+N_2 mixture.

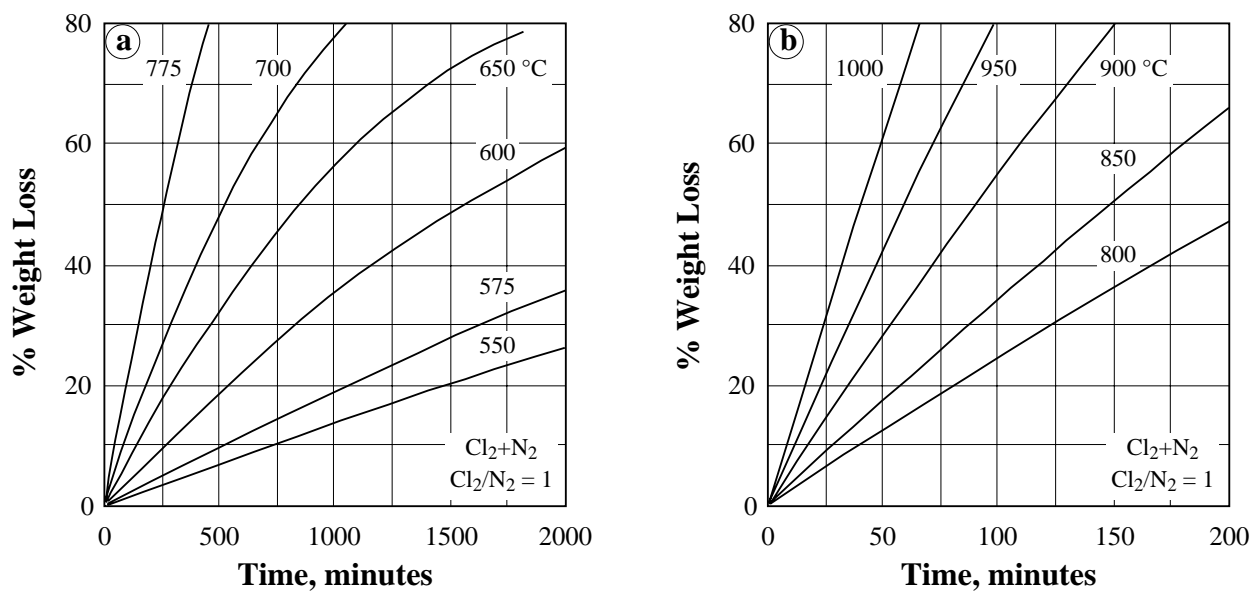


Fig. 4- Isotherms of chlorination of Cr_2O_3 with Cl_2+N_2 for (a) $T \leq 775$ °C and (b) $T \geq 800$ °C.

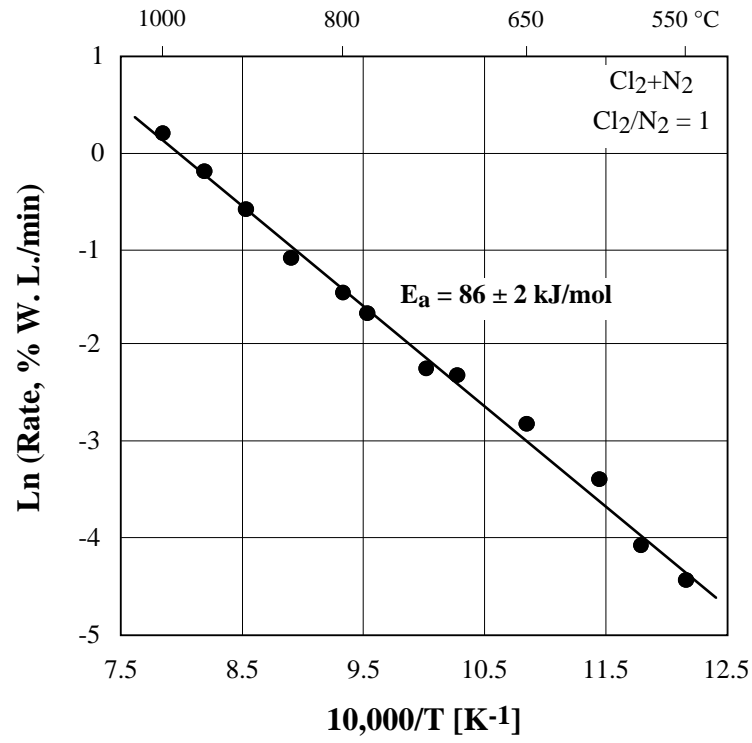


Fig. 5- Arrhenius plot of chlorination of Cr_2O_3 by Cl_2+N_2 .

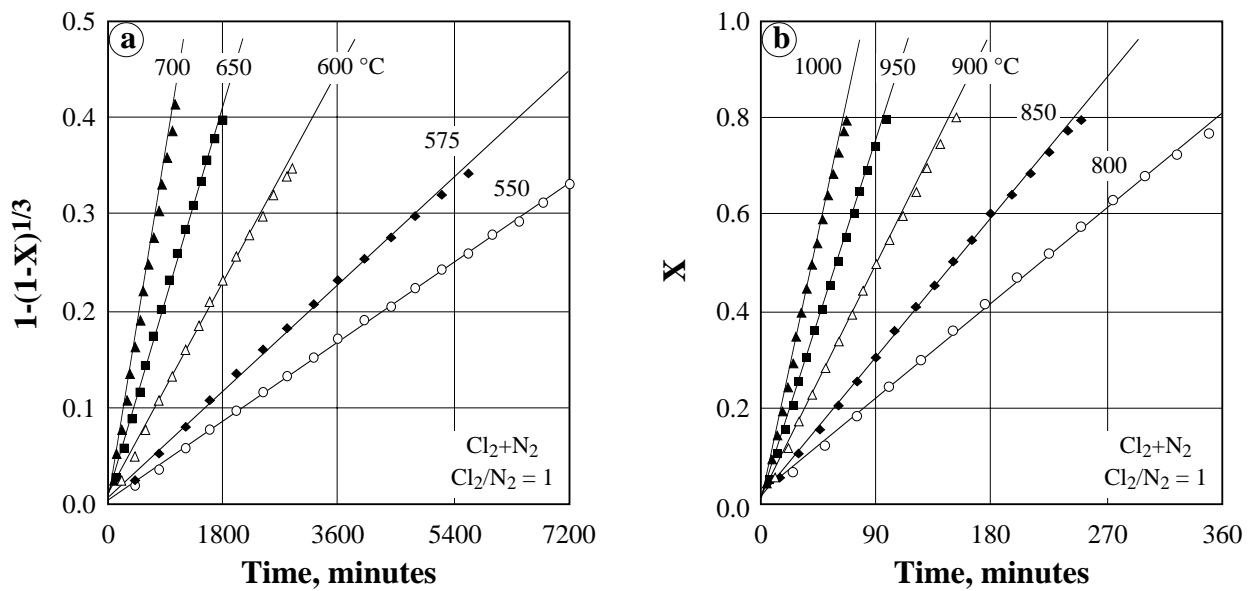


Fig. 6- Mathematical fitting of the chlorination data at (a) $T \leq 700$ °C using Eq. 14 and (b) $T \geq 800$ °C using Eq. 12.

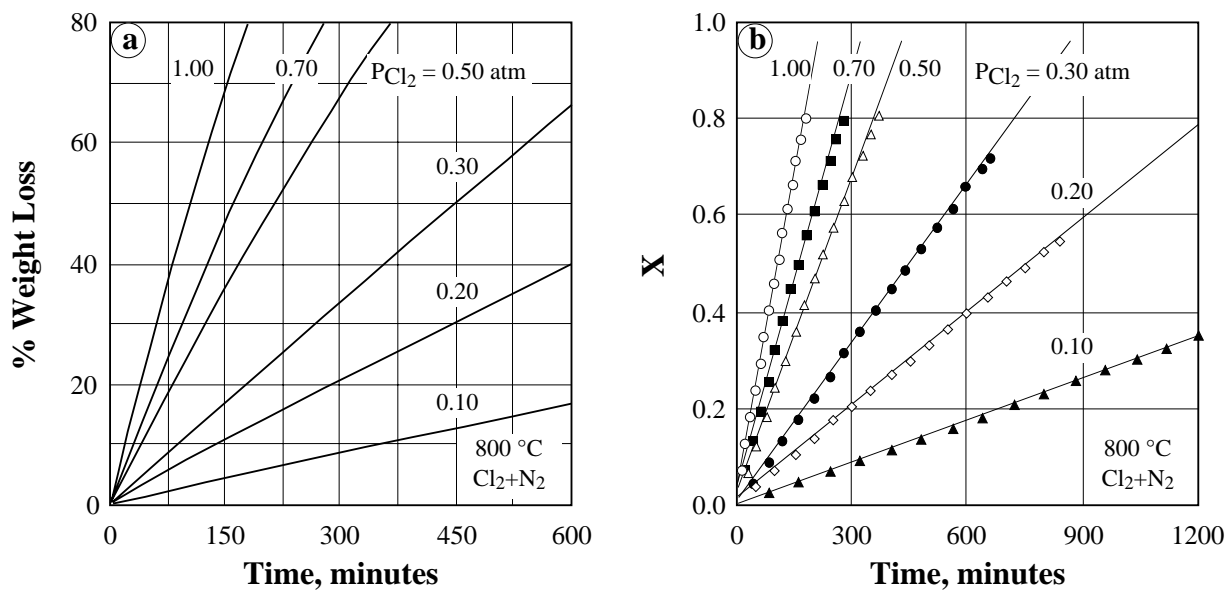


Fig. 7- Isotherms of chlorination of Cr_2O_3 (a) using different chlorine pressures and (b) linearization of data using Equation 12.

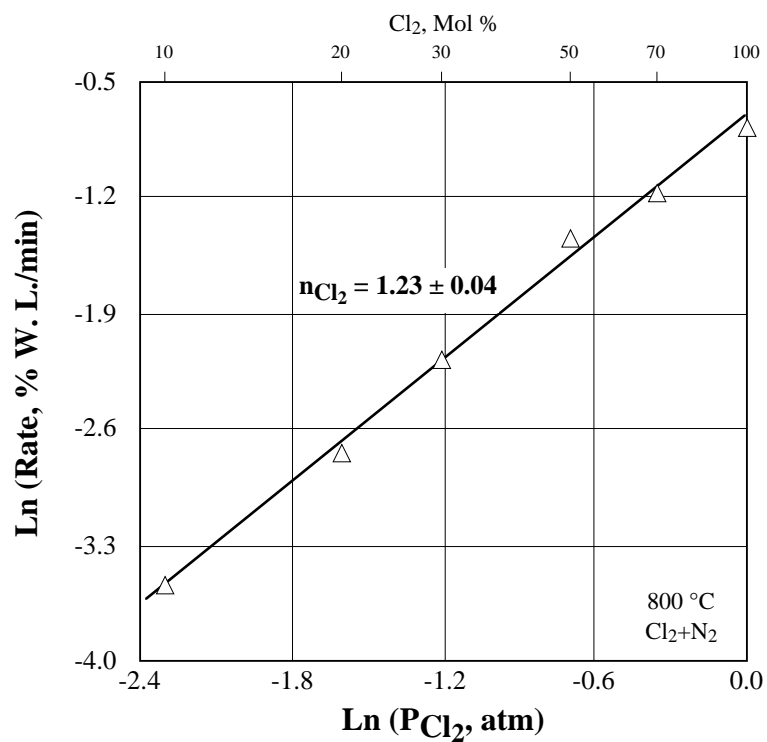


Fig. 8- Apparent reaction order of Cr_2O_3 chlorination with respect to chlorine.

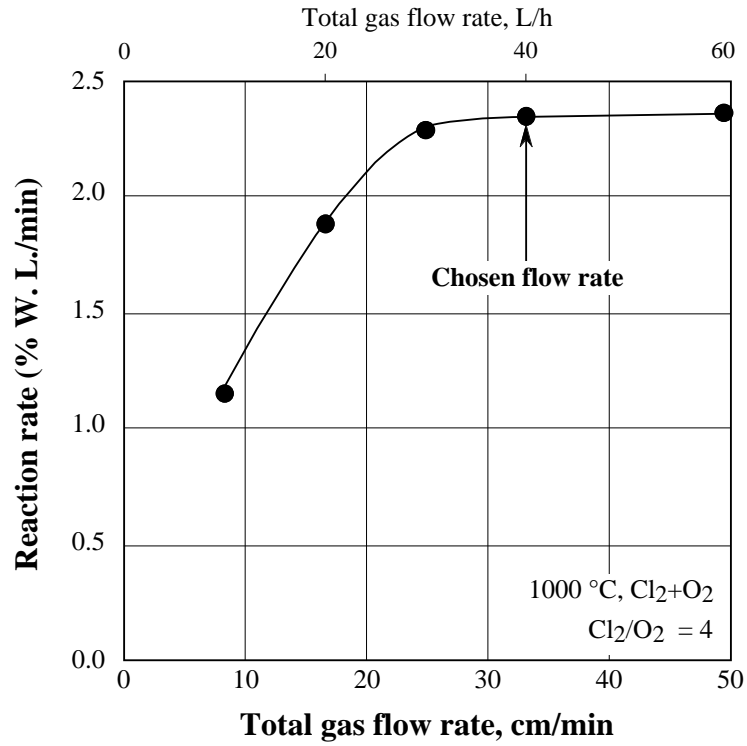


Fig. 9- Chlorination rate of Cr₂O₃ as a function of flow rate of the Cl₂+O₂ mixture.

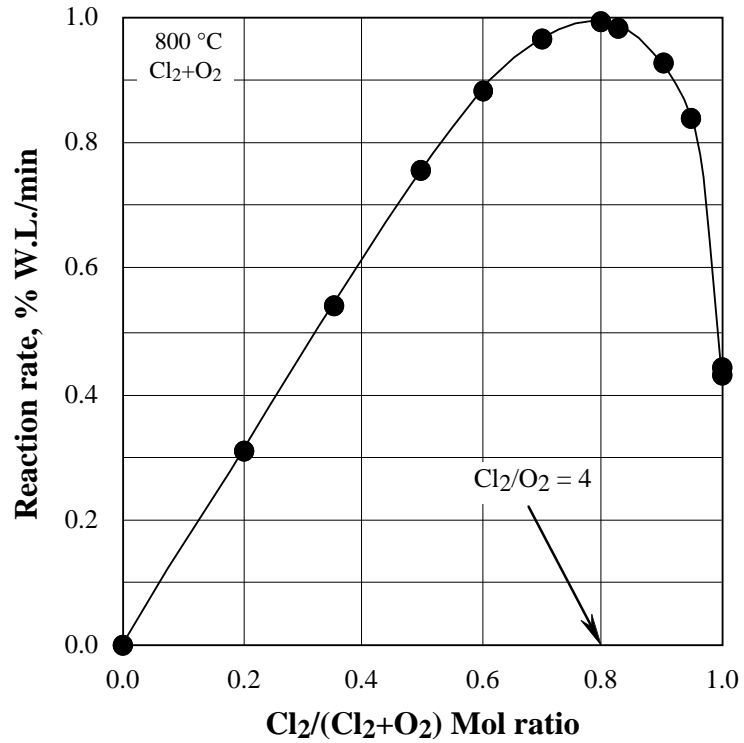


Fig. 10- Effect of Cl₂/(Cl₂+O₂) molar ratio on the reaction rate of Cr₂O₃ oxychlorination.

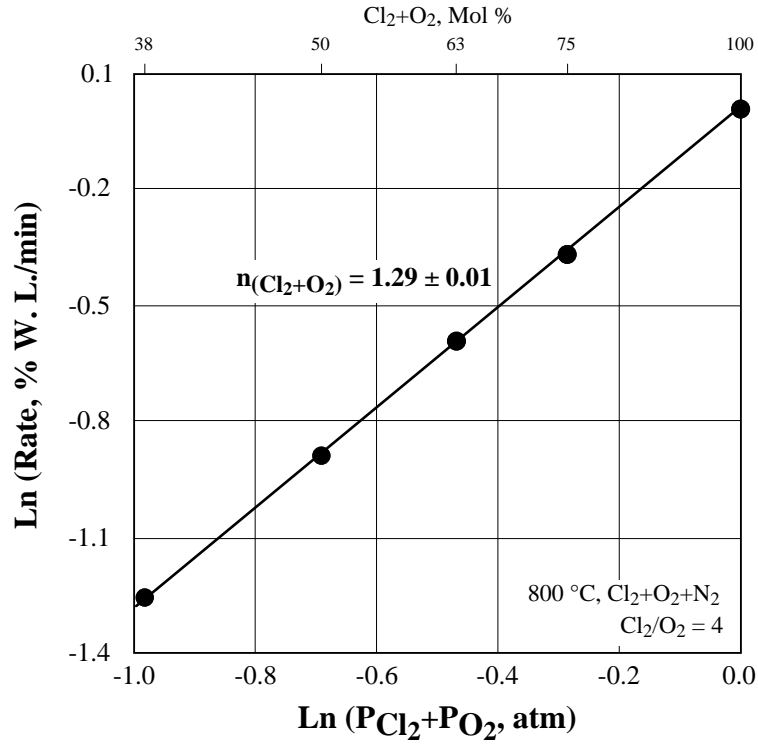


Fig. 11- Apparent reaction order with respect to Cl_2+O_2 .

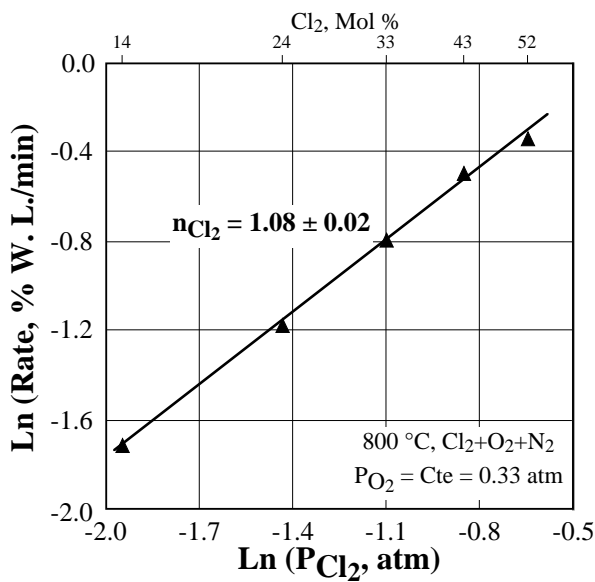


Fig. 12- Apparent reaction order with respect to Cl_2 .

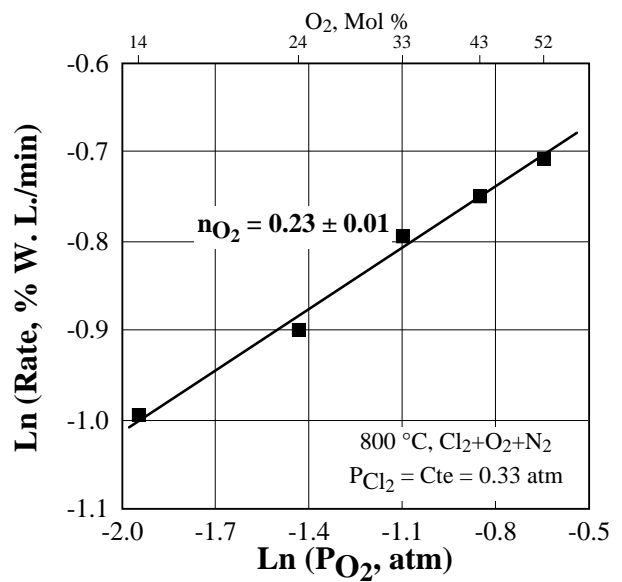


Fig. 13- Apparent reaction order with respect to O_2 .

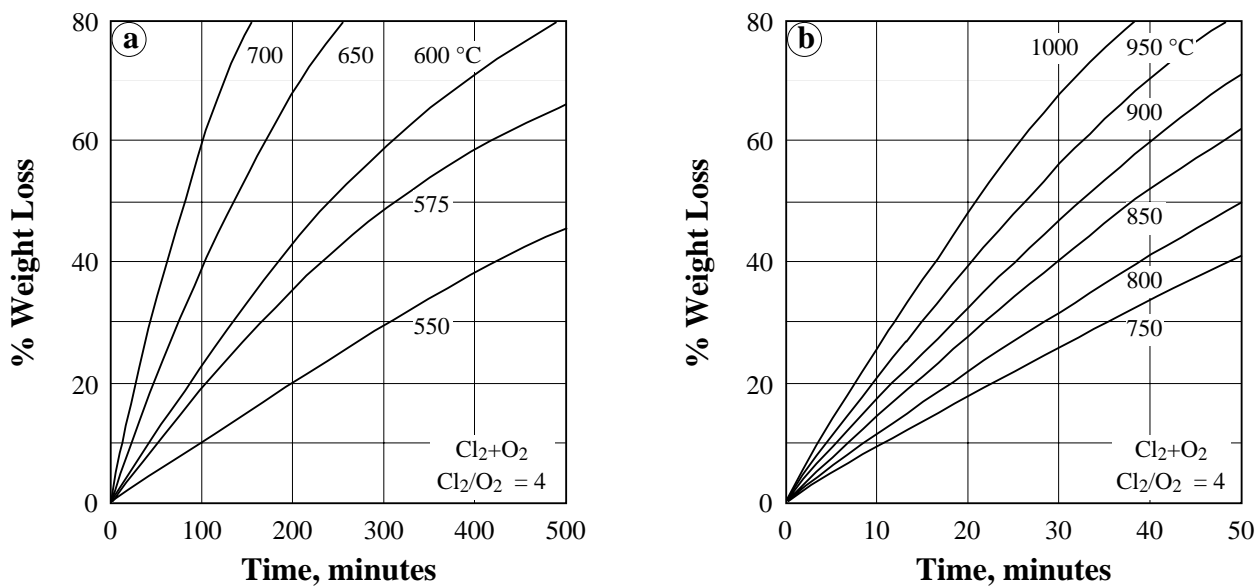


Fig. 14- Isotherms of chlorination of Cr_2O_3 with Cl_2+O_2 for (a) $T \leq 700$ °C and (b) $T \geq 750$ °C.

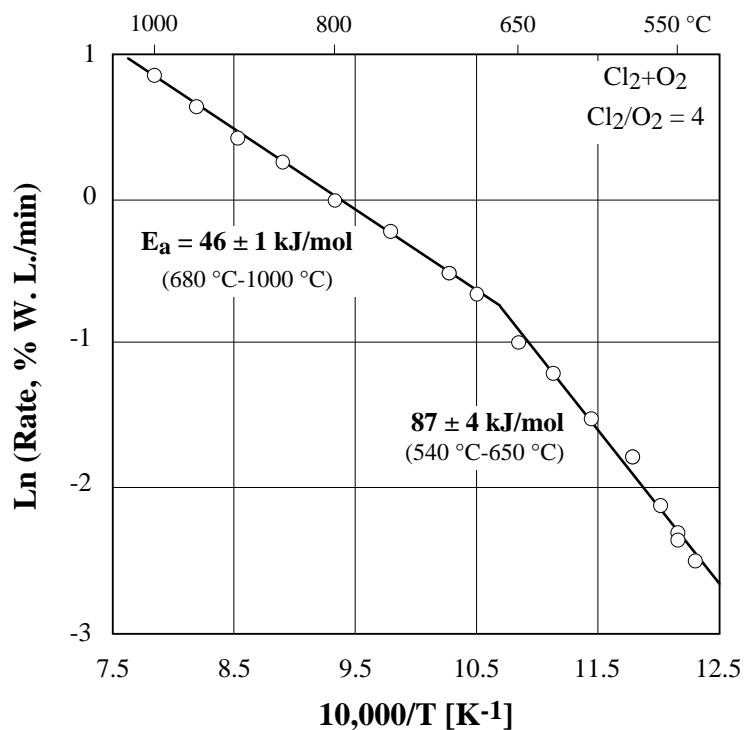


Fig. 15- Arrhenius plot of chlorination of Cr_2O_3 by Cl_2+O_2 .

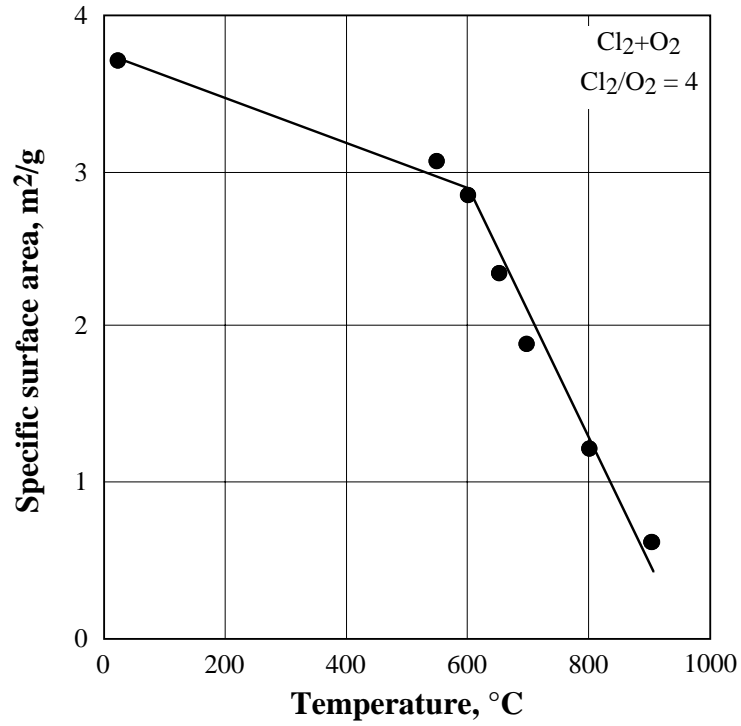


Fig. 16- Evolution of the specific surface area of partially oxychlorinated samples ($X \approx 0.27$) of Cr_2O_3 as a function of temperature.

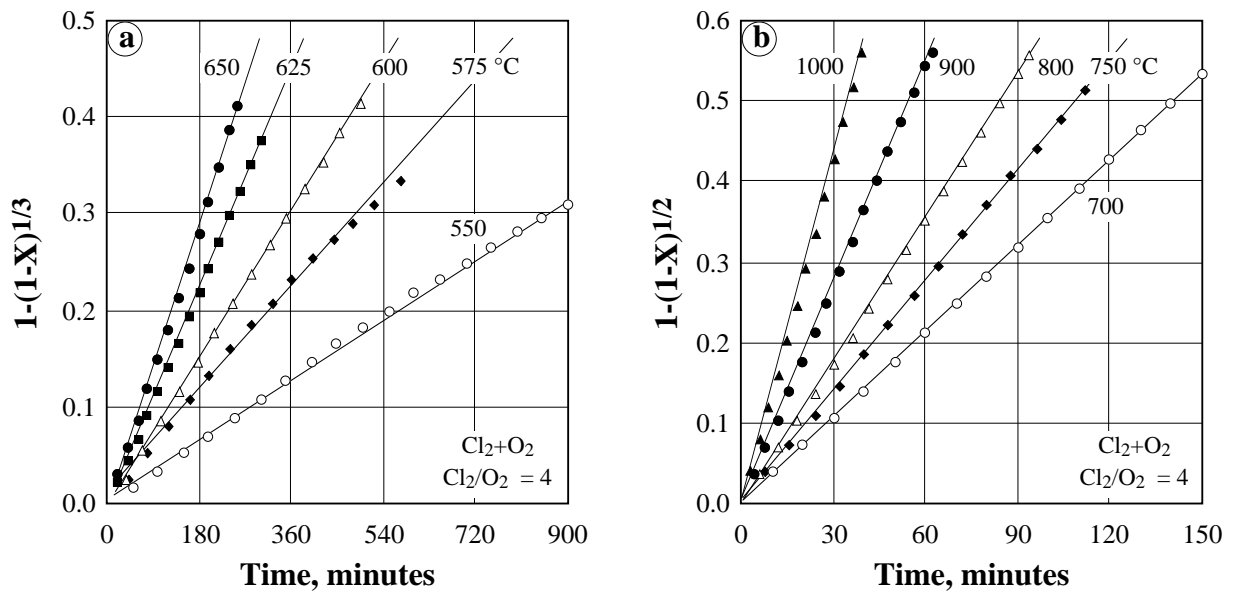


Fig. 17- Mathematical fitting of the oxychlorination data at (a) $T \leq 650^\circ\text{C}$ and (b) $T \geq 700^\circ\text{C}$ using Eqs 14 and 13, respectively.

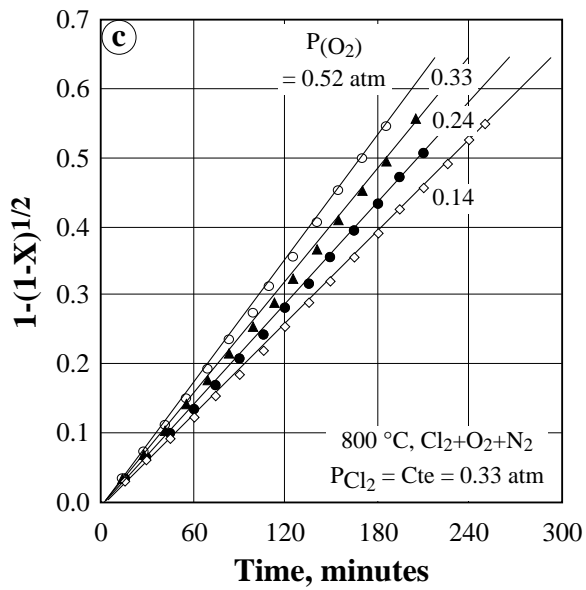
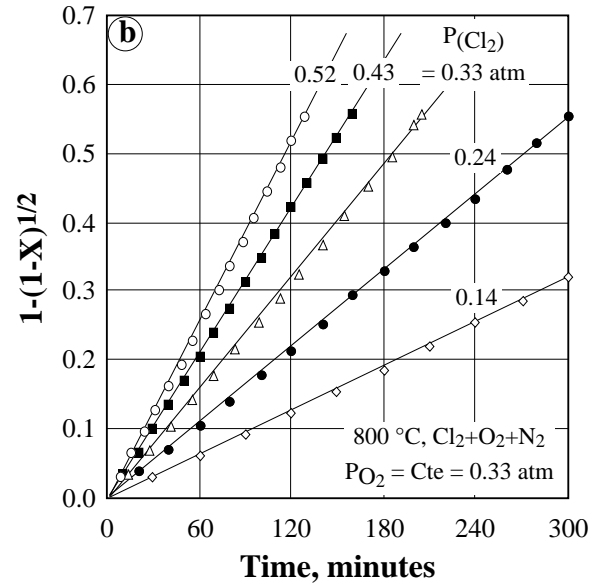
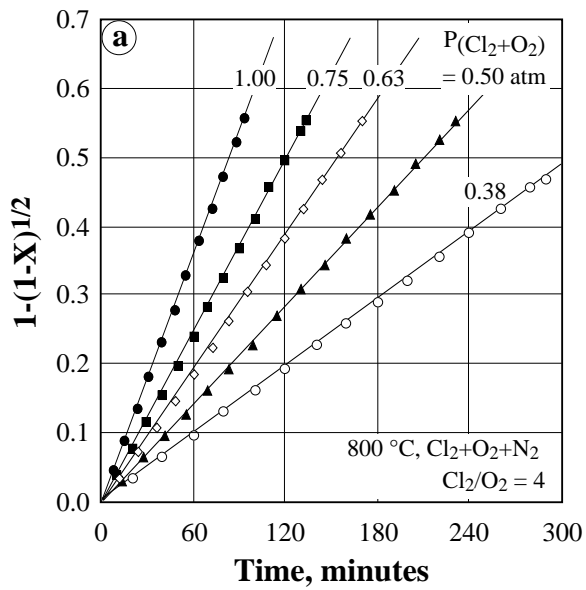


Fig. 18- Mathematical fitting of the oxychlorination data at $800\text{ }^\circ\text{C}$ using Eq 13 :

- (a) for different (Cl_2+O_2) partial pressure,
- (b) for different Cl_2 partial pressure,
- (c) for different O_2 partial pressure.

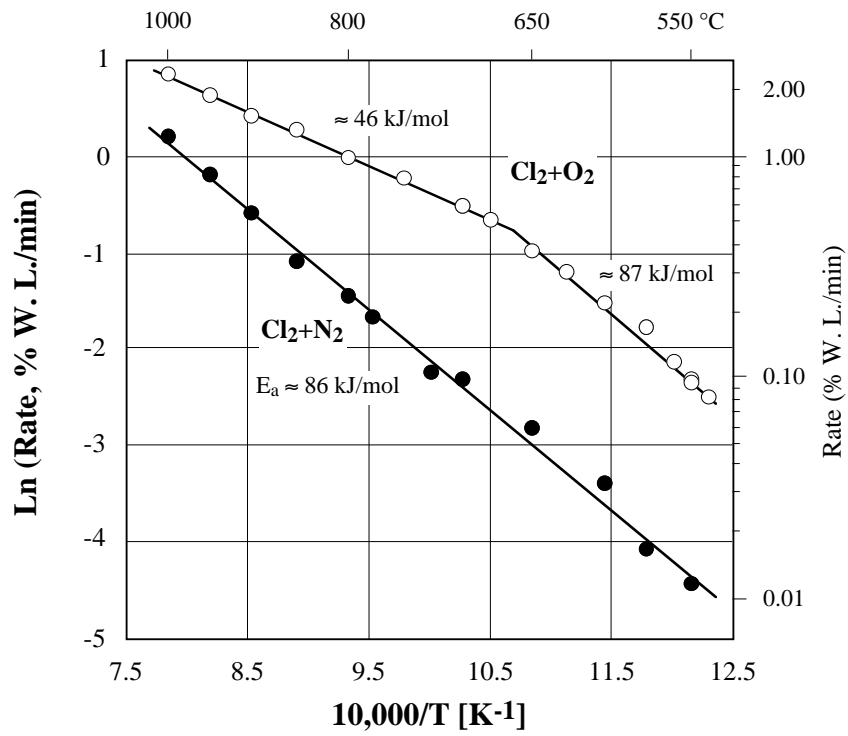


Fig. 19- Comparison of Arrhenius plots of chlorination and oxychlorination of Cr_2O_3 .