

How to efficiently extract phenolic compounds from lignin bio-oil ?

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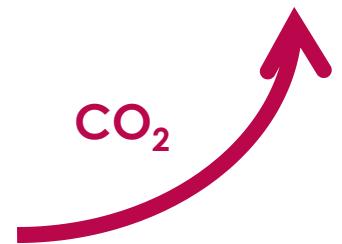


Context



Global warming

CO₂

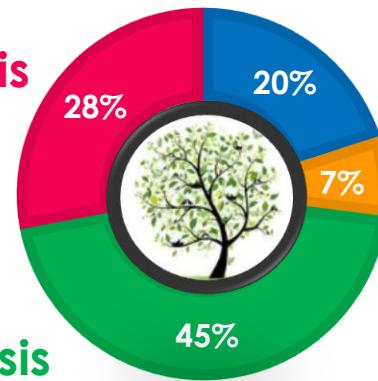


Context

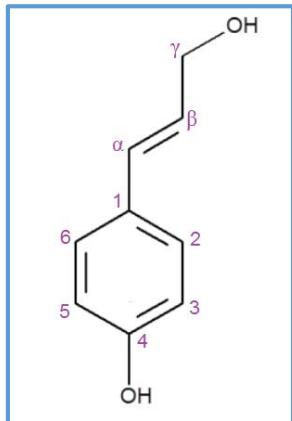
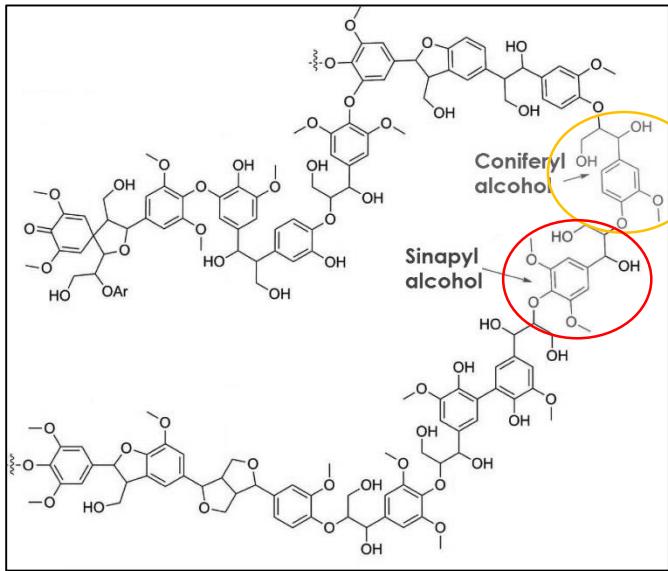


Hemicellulosis

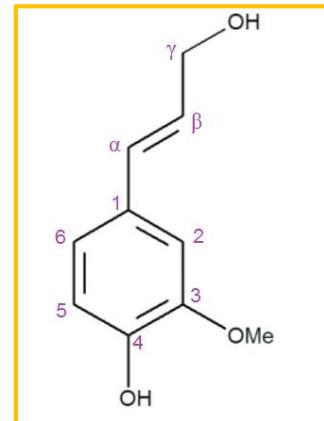
Cellulosis



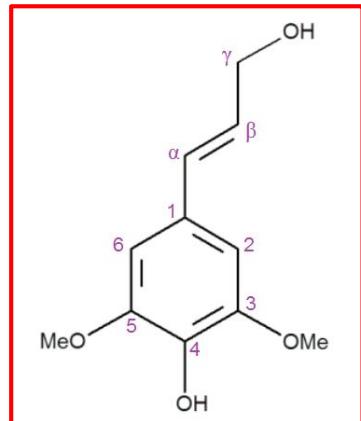
Lignin's structure



p-coumaryl alcohol

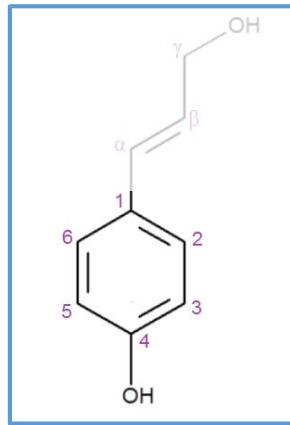
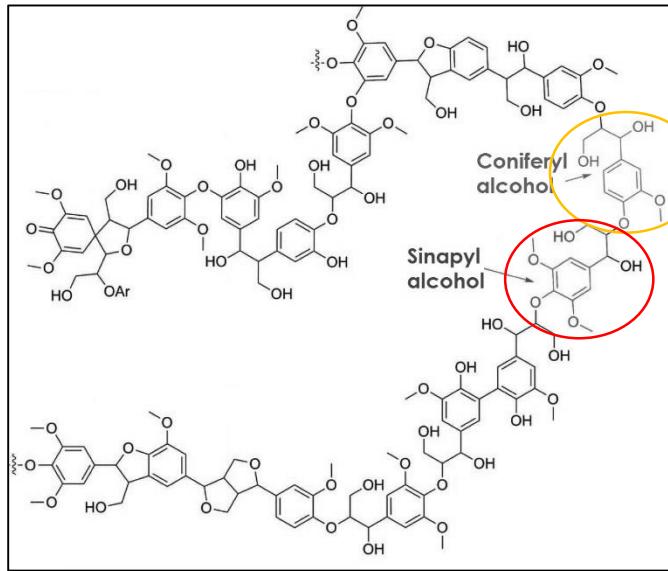


coniferyl alcohol

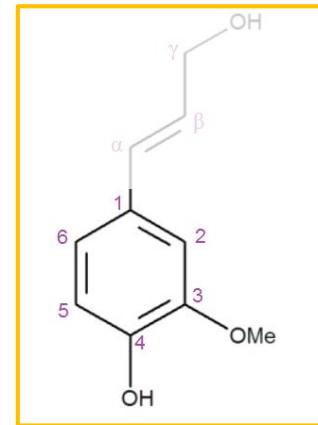


sinapyl alcohol

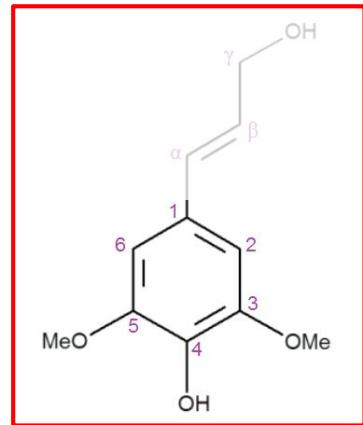
Lignin's structure



p-coumaryl alcohol
↓
p-hydroxyphenyl unit

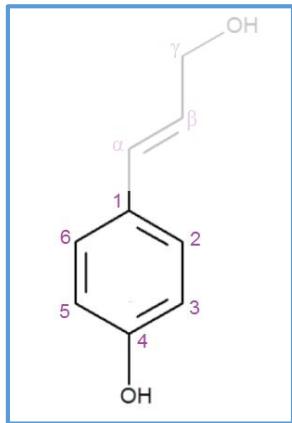
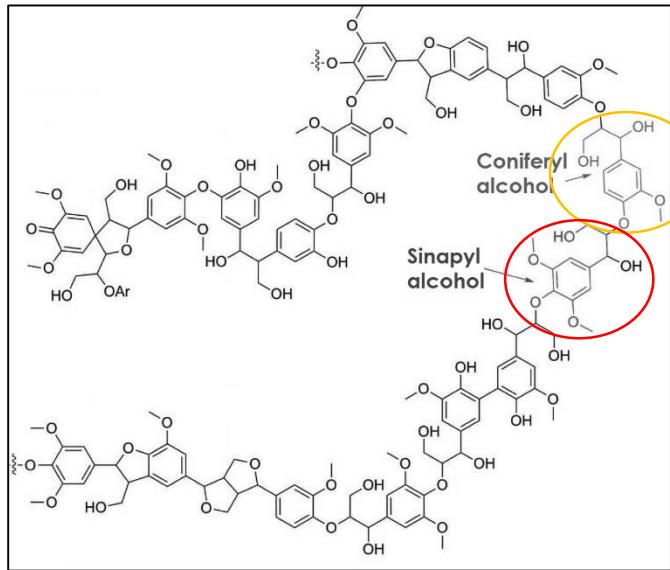


coniferyl alcohol
↓
guaiacyl unit

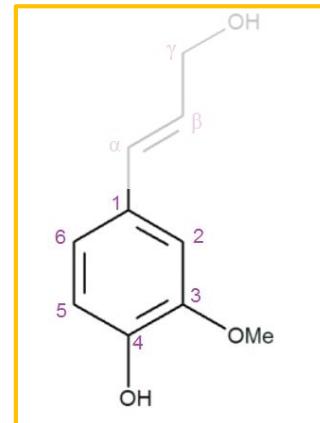


sinapyl alcohol
↓
sinapyl unit

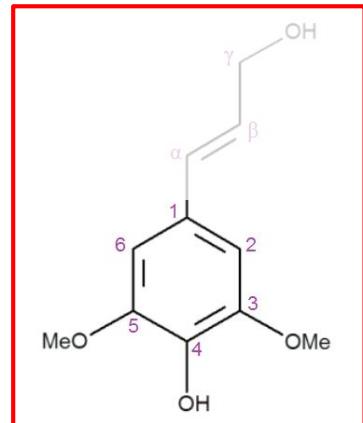
Lignin's structure



p-coumaryl alcohol
↓
p-hydroxyphenyl unit



coniferyl alcohol
↓
guaiacyl unit

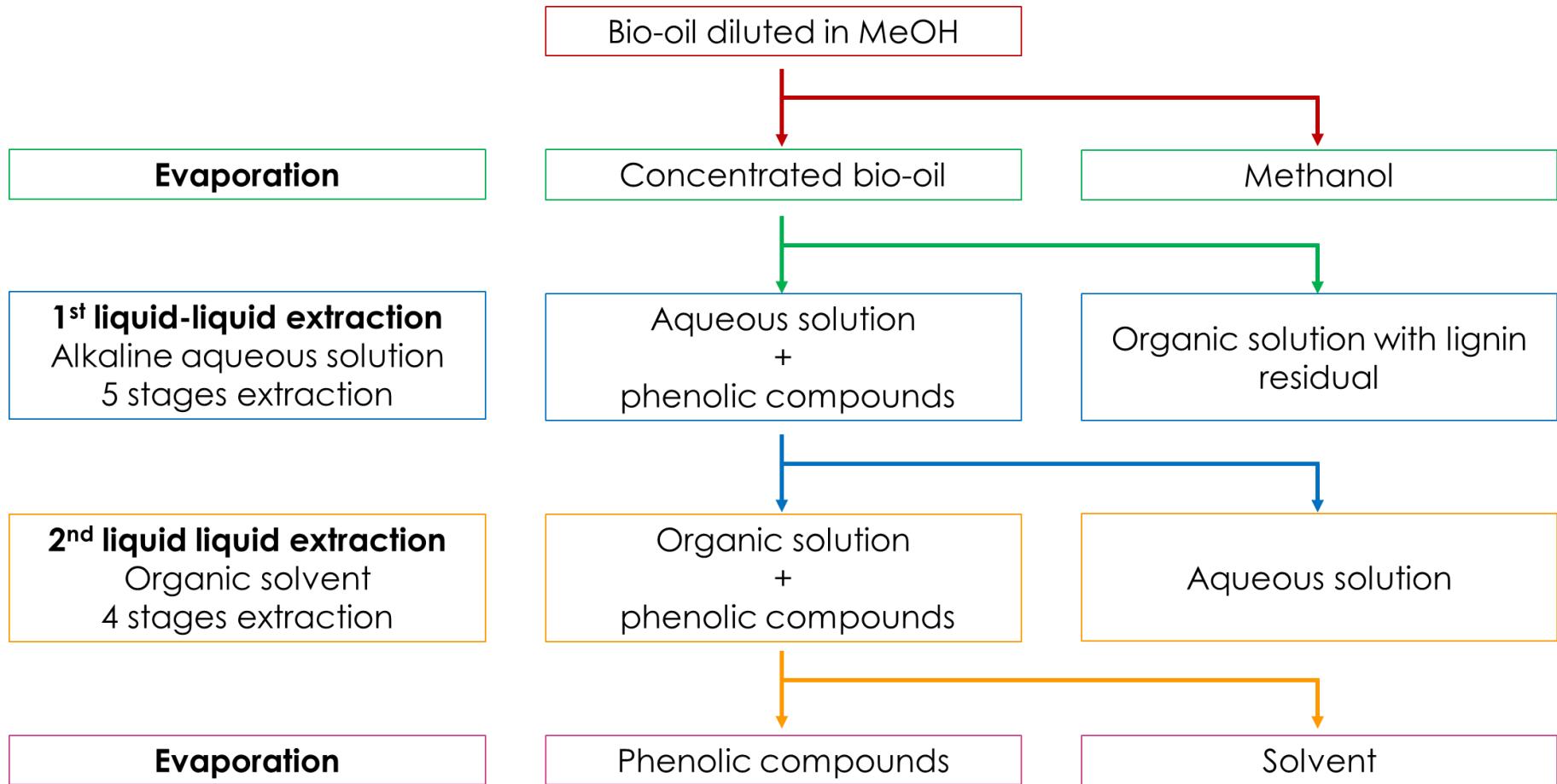


sinapyl alcohol
↓
sinapyl unit

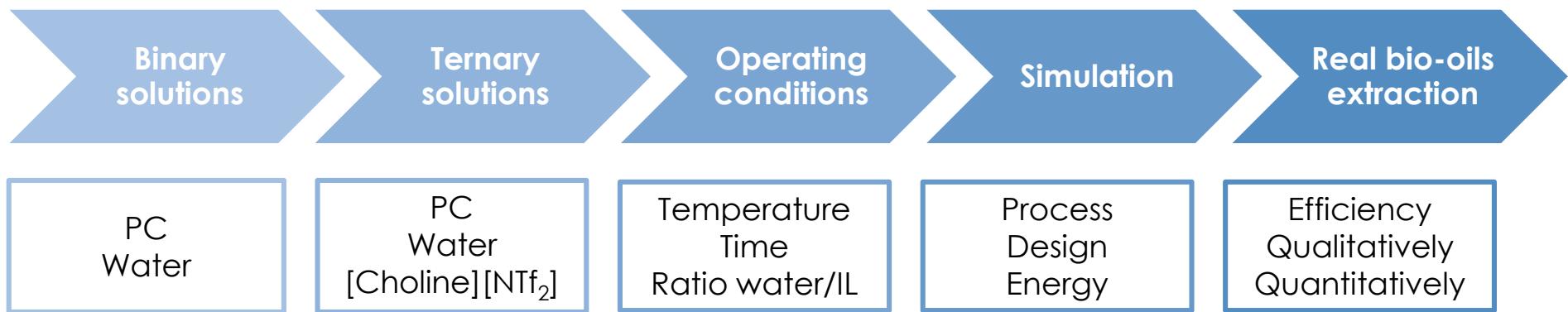


Flash pyrolysis
High temperature - Low residence time

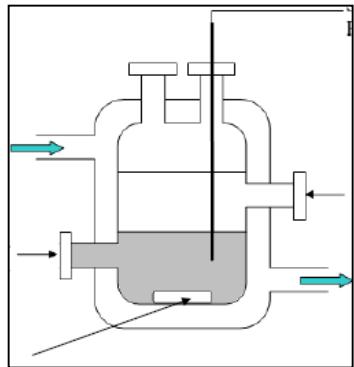
Extraction process



Plan



Binary solutions (PC + water)



Shake Flask method

Jacketed glass cell + Thermostatic bath
Stirring + Settling down
Analysis by UV spectroscopy

Solid-liquid equilibria

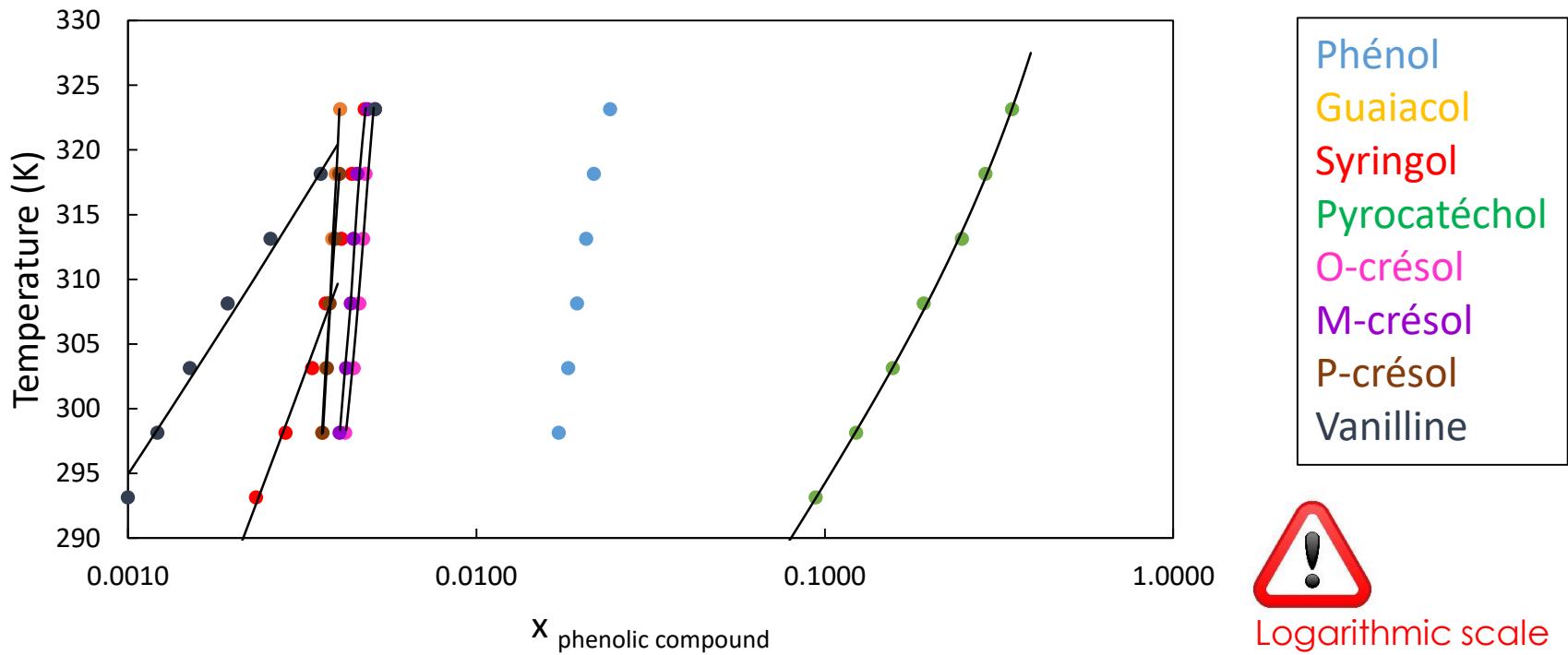
Syringol - water
Pyrocatechol - water
Vanillin - water

Liquid-liquid equilibria

Phenol - water
Guaiacol- water
O-cresol- water
M-cresol - water
P-cresol - water

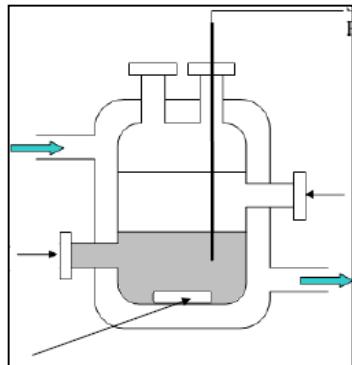
Reference : Phase equilibria of phenolic compounds in water or ethanol; L Cesari,
S Namysl, L Canabady-Rochelle, F Mutelet; Fluid Phase Equilibria 453, 58-66

Binary solutions (PC + water)



Determination of the interaction parameters of the NRTL model
Relative deviation on x < 1%

Ternary solutions (25°C)



Shake Flask method

Jacketed glass cell + Thermostatic bath

Stirring + Settling down

Analysis by gas chromatography

- Thermal Conductivity Detector
- Flame Ionization Detector

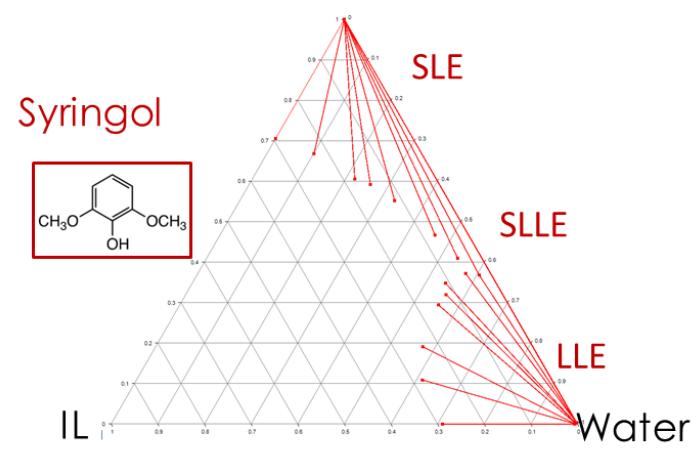
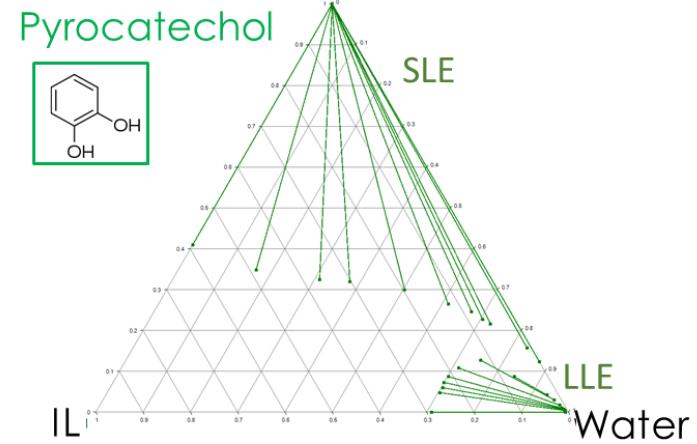
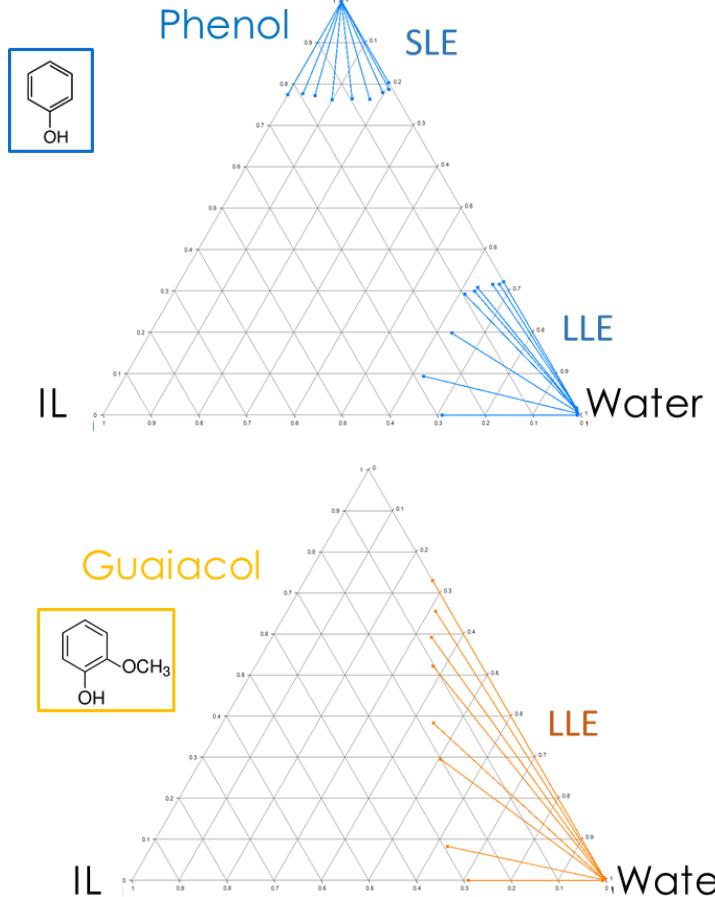


3 Compounds

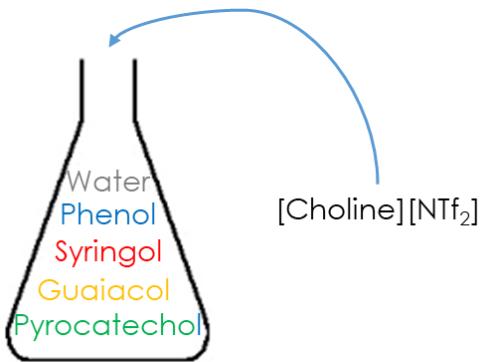
- Phenolic compound
- Water
- [Choline][Ntf₂]

Reference : Extraction of phenolic compounds from aqueous solution using choline bis (trifluoromethylsulfonyl) imide; L Cesari, L Canabady-Rochelle, F Mutelet; Fluid Phase Equilibria 446, 28-35

Ternary diagrams (25°C)



Influence of parameters



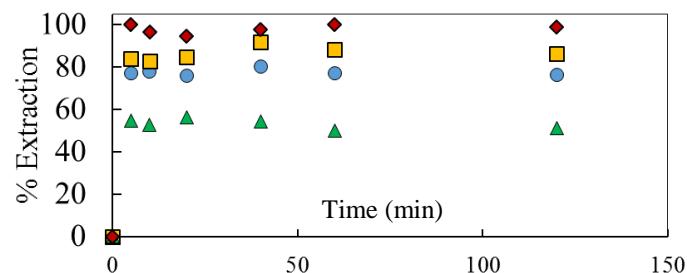
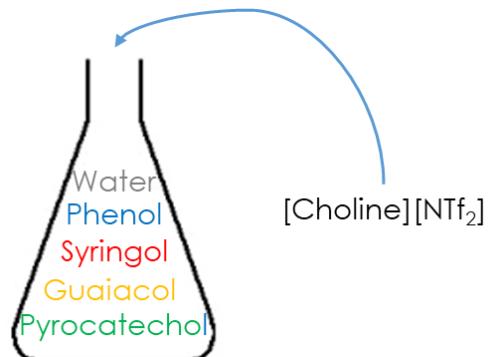
Parameters :

Time (0-6H)

Influence of **Temperature** (25-45°C)

Influence of **Ratio IL/water** (0.5-1-2)

Influence of parameters

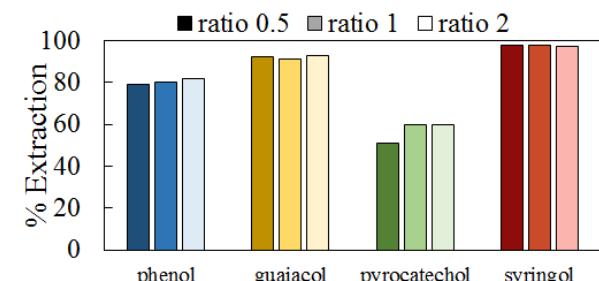
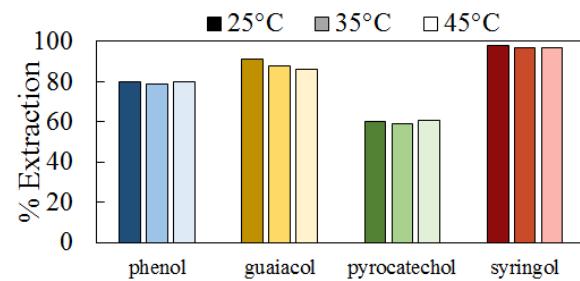


Parameters :

Time (0-6H)

Influence of **Temperature** (25-45°C)

Influence of **Ratio IL/water** (0.5-1-2)



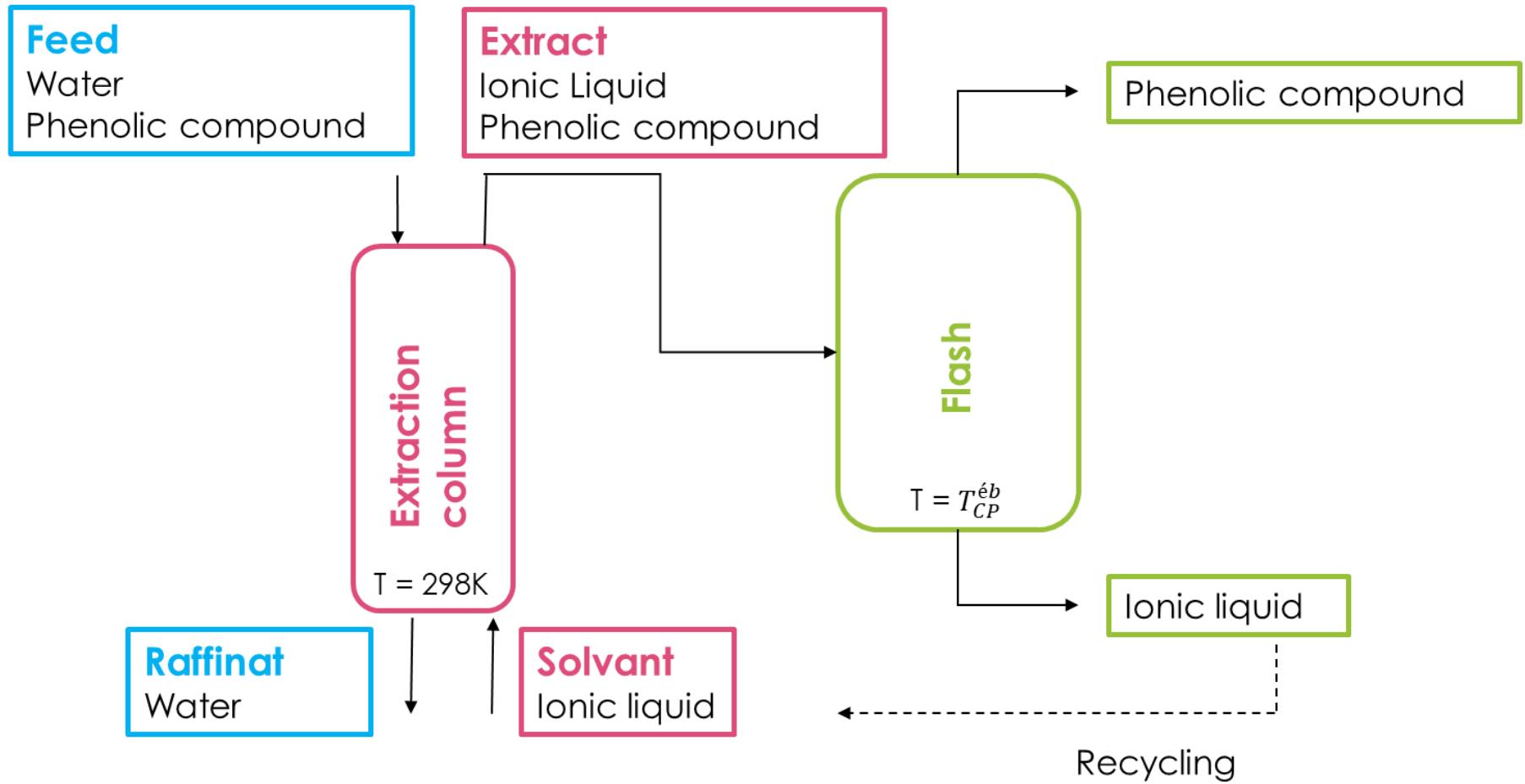
Results :

The liquid-liquid equilibria is reached quickly (< 5 minutes)

The temperature does not influence the LLE

The IL / water mass ratio has practically no influence on the extraction

Modelisation / Simulation



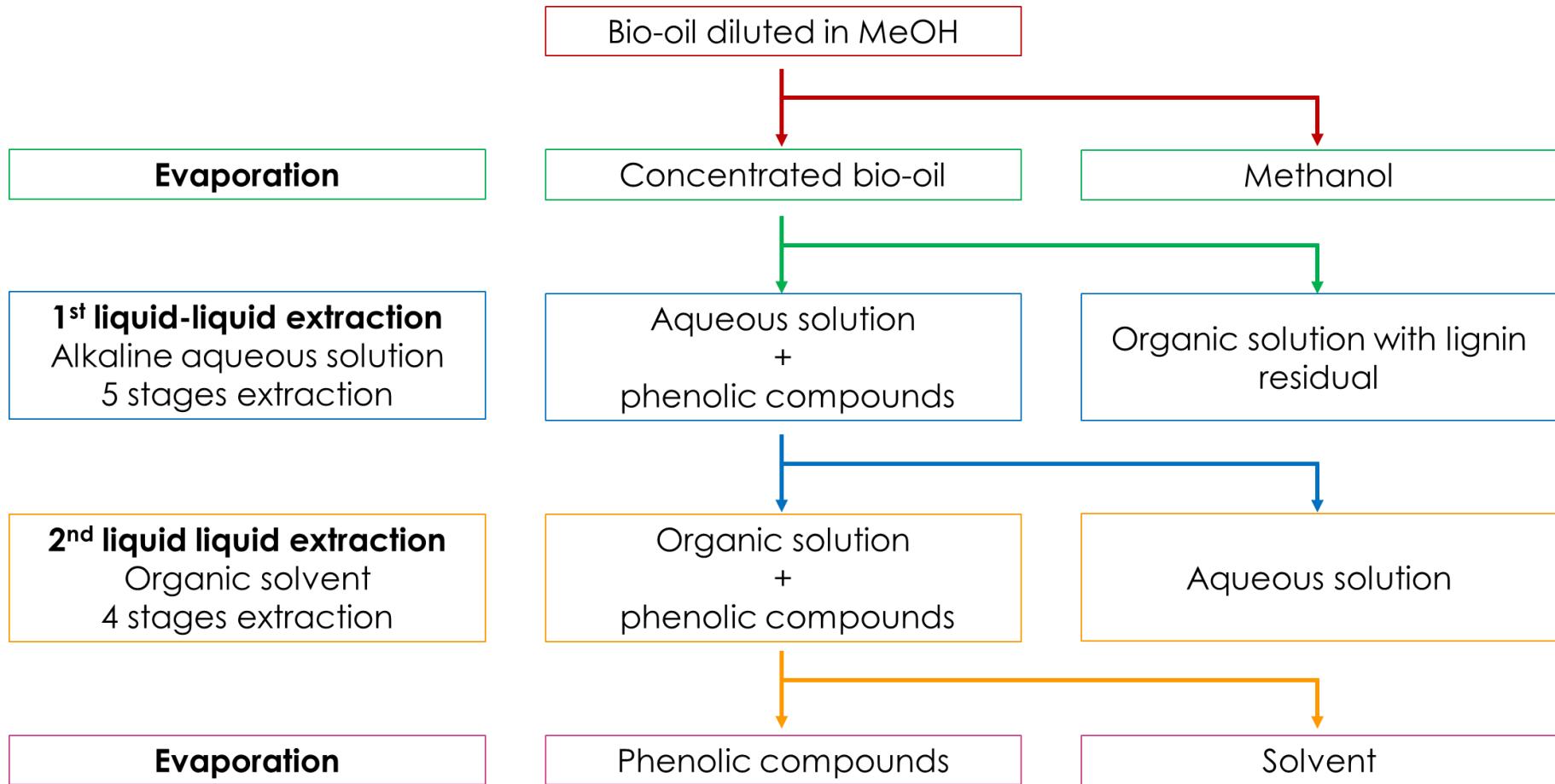
Modelisation

Hypothesis

- Counter-flow at 298.15K
- Mass fraction of phenolic compound in feed: 0.015
- Resulting extract and raffinate flows approximately equal the solvent and feed flows respectively
- Extraction effective at a 99.995% rate

| Results | | | | |
|------------------------------|--------------------------------|-------------------------------|------------------------------------|----------------------------|
| Solvent | Compound | <i>Solvent Feed</i> ratio | Number of theoretical steps | Energy (MJ/kg compound) |
| [Choline][NTf ₂] | Phenol | 0.3 | 7 | 10.75 |
| | Guaiacol | 0.3 | 4 | 3.41 |
| | Syringol | 0.1 | 7 | 6.57 |
| | Pyrocatechol | 1.3 | 7 | 45.64 |
| Ethyl acetate | Guaiacol (X.Li et al. 2016) | | 3 (extraction) 8 (distillation) | 12.42 |

Extraction process



Real bio-oils extractions



| Solvent |
|--------------------------|
| Compounds |
| Phenol |
| O-cresol |
| P-cresol |
| Guaiacol |
| 4-ethylphenol |
| 2-methoxy-3-methylphenol |
| 2-methoxy-4-vinylphenol |
| Syringol |

Separation of phenols from lignin pyrolysis oil using ionic liquid; L Cesari, L Canabady-Rochelle, F Mutelet;
Separation and Purification Technology 209, 528-534

Real bio-oils extractions



| Solvent | Ionic Liquid | | |
|--------------------------|----------------------|----------------------|----------------|
| Compounds | 1 st wash | 2 nd wash | Total 2-stages |
| Phenol | 69 | 21 | 90 |
| O-cresol | 55 | 13 | 68 |
| P-cresol | 63 | 13 | 76 |
| Guaiacol | 68 | 19 | 87 |
| 4-ethylphenol | 92 | n.d. | 92 |
| 2-methoxy-3-methylphenol | 41 | n.d. | 41 |
| 2-methoxy-4-vinylphenol | 89 | 11 | 100 |
| Syringol | 80 | 20 | 100 |

Separation of phenols from lignin pyrolysis oil using ionic liquid; L Cesari, L Canabady-Rochelle, F Mutelet;
Separation and Purification Technology 209, 528-534

Real bio-oils extractions



| Solvent | Ionic Liquid | | | Ethyl acetate |
|--------------------------|----------------------|----------------------|----------------|----------------|
| Compounds | 1 st wash | 2 nd wash | Total 2-stages | Total 4-stages |
| Phenol | 69 | 21 | 90 | 83 |
| O-cresol | 55 | 13 | 68 | 58 |
| P-cresol | 63 | 13 | 76 | 81 |
| Guaiacol | 68 | 19 | 87 | 89 |
| 4-ethylphenol | 92 | n.d. | 92 | 70 |
| 2-methoxy-3-methylphenol | 41 | n.d. | 41 | 28 |
| 2-methoxy-4-vinylphenol | 89 | 11 | 100 | 96 |
| Syringol | 80 | 20 | 100 | 72 |

Separation of phenols from lignin pyrolysis oil using ionic liquid; L Cesari, L Canabady-Rochelle, F Mutelet;
Separation and Purification Technology 209, 528-534

Conclusion

Thermodynamique study

Experimental measurements

Determination of parameters for thermodynamic models

Extraction

Quick and efficient at room temperature

Requires a few amount of ionic liquid

Process design

Creation of a simpler process

Design of smaller units

Lower energy consumption

Real study case

Confirmation of the [Choline][NTf₂] extraction efficiency

Thank you

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