

# Kinetic parameters for the thermal cracking of simple hydrocarbons: From laboratory to geological time-temperature conditions

V. Burklé-Vitzthum, R. Bounaceur, Raymond Michels, G. Scacchi, P.-M.

Marquaire

# ▶ To cite this version:

V. Burklé-Vitzthum, R. Bounaceur, Raymond Michels, G. Scacchi, P.-M. Marquaire. Kinetic parameters for the thermal cracking of simple hydrocarbons: From laboratory to geological time-temperature conditions. Journal of Analytical and Applied Pyrolysis, 2017, 125, pp.40-49. 10.1016/j.jaap.2017.04.020. hal-03554606

# HAL Id: hal-03554606 https://hal.univ-lorraine.fr/hal-03554606v1

Submitted on 3 Feb 2022

**HAL** is a multi-disciplinary open access archive for the deposit and dissemination of scientific research documents, whether they are published or not. The documents may come from teaching and research institutions in France or abroad, or from public or private research centers. L'archive ouverte pluridisciplinaire **HAL**, est destinée au dépôt et à la diffusion de documents scientifiques de niveau recherche, publiés ou non, émanant des établissements d'enseignement et de recherche français ou étrangers, des laboratoires publics ou privés.

### **1 KINETIC PARAMETERS FOR THE THERMAL CRACKING OF**

# 2 SIMPLE HYDROCARBONS: FROM LABORATORY TO 3 GEOLOGICAL TIME-TEMPERATURE CONDITIONS

4 V. Burklé-Vitzthum<sup>a,\*</sup>, R. Bounaceur<sup>a</sup>, R. Michels<sup>b</sup>, G. Scacchi<sup>a</sup>, P.-M. Marquaire<sup>a</sup>

<sup>5</sup> <sup>a</sup> Laboratory of Reactions and Process Engineering, LRGP UMR 7274, CNRS, Université de

6 Lorraine BP 20451, 54001 Nancy, France

<sup>b</sup> GeoRessources UMR 7359, CNRS, Université de Lorraine BP 70239, 54501 Vandœuvre-

8 lès-Nancy, France

9 Corresponding author: valerie.vitzthum@univ-lorraine.fr

#### 10 Abstract

Apparent kinetic parameters (frequency factor A and activation energy  $E_a$ ) were computed at 11 700 bar and two temperatures: 200°C, a characteristic of deeply buried reservoirs of 12 petroleum and 400°C an average temperature used for laboratory pyrolysis to simulate 13 thermal cracking of petroleum. Several hydrocarbons were studied by simulation: several 14 linear alkanes and one branched alkane, toluene, 2-methylnaphthalene, 1-,3-,5-15 trimethylbenzene, methylcyclohexane, butylcyclohexane, tetralin and decylbenzene. The 16 calculations were performed using detailed kinetic models (mostly free-radical mechanisms) 17 previously constructed. The computation of  $E_a$  does not depend on the global rate law, but we 18 assumed a first-order reaction law to compute A. The apparent kinetic parameters of all 19 hydrocarbons are slightly modified by temperature and rather strongly for tetralin and 20 decylbenzene. The deviation, due to the use of Arrhenius law with the apparent kinetic 21 parameters computed at 400°C for extrapolation to geological temperature, is important in 22 most cases, even if the kinetic parameters do not strongly depend on temperature. In this 23 study, most hydrocarbons appear more stable at 200°C than it could be inferred by using the 24 extrapolation of the Arrhenius law from 400°C to 200°C, except for tetralin and decylbenzene 25 26 which appear more reactive. The apparent kinetic parameters that were computed at 200°C 27 could be implemented in global kinetic models used for the assessment of reservoirs.

#### 28 **1. Introduction**

The prediction of the petroleum composition, submitted to thermal cracking over millions of 29 years, requires a good knowledge of the reaction kinetics, particularly in deeply buried 30 reservoirs, at high pressure (100-1000 bar) and high temperature (> 200°C). The apparent 31 kinetic parameters (apparent frequency factor A and apparent activation energy  $E_a$ ) are 32 commonly determined via pyrolysis in laboratory at high pressure of crude oils [i.e.1-13] or 33 pure hydrocarbons [i.e. 14-24]. The geological time is compensated by higher temperatures 34 (350-450°C) than those encountered in reservoir. The bulk kinetic models derived from 35 experimental results are then computed using geological time-temperature conditions. Due to 36 the complexity of the chemical composition of crude oils, it is easier to derive reliable kinetic 37 parameters from pyrolysis of pure hydrocarbons or simple mixtures. 38

In order to determine precisely the main reaction pathways and obtain reliable predictions, 39 detailed kinetic models for the thermal reaction of pure hydrocarbons or simple mixtures can 40 also be set up. These detailed kinetic models consist of mechanisms made of elementary steps 41 (mainly free-radical reactions) with their fundamental kinetic parameters [25-37]. That is the 42 reason why they can be extrapolated in the pressure and temperature ranges of 100-1000 bar 43 and 150-450°C, respectively: the main reaction pathways and the fundamental kinetic 44 parameters remain unchanged. The main advantages of these models are their precision and 45 the possibility for extrapolation. However, the main drawback is the size of the model (several 46 47 hundred even thousand reactions) which prevents their integration in a basin model.

This paper aims to test if the apparent kinetic parameters are constant in the temperature range 48 of 200-400°C, at high pressure, i.e. testing if the apparent kinetic parameters computed at 49 400°C can be used at 200°C by extrapolation of the Arrhenius law in a reliable manner. A 50 51 temperature equals to 200°C is typical of deeply buried oil reservoirs, and 400°C is an average temperature for laboratory pyrolysis. In this study, the selected hydrocarbons are 52 linear and branched alkanes, several aromatic compounds (toluene, trimethylbenzene "TMB", 53 "MN", decylbenzene "DB" and methylnaphthalene tetralin) and cycloalkanes 54 (methylcyclohexane "MCH" and butylcyclohexane "BCH"). All free-radical mechanisms 55 mentioned in this paper were constructed and validated based on experimental database 56 recovered by our team for about 15 years ([25-28], [30-32], [34-35]). The detailed models are 57 used to compute the apparent kinetic parameters at 700 bar and two temperatures: 200°C and 58

400°C. The kinetic parameters computed at 400°C and then 200°C are used to calculate and 59 compare the conversion after 1, 10 or 100 million years at 200°C (depending on the reactivity 60 of the compound), as well as the half-life. The relative scale of stability is set up and 61 compared at both temperatures. This comparison is performed to highlight the influence of 62 extrapolating kinetic parameters outside the range of temperatures in which they were 63 computed. This work is the first step of the construction of bulk kinetic models reliable in the 64 geological pressure and temperature conditions, and which could be implemented in complete 65 basin models for petroleum exploration purposes. 66

67

#### 2. Methodology for the determination of apparent kinetic parameters

Apparent kinetic parameters were first calculated at  $T_0 = 400^{\circ}$ C and then 200°C, at 700 bar. The computation of the apparent activation energy does not depend on the kinetic law, when it can be done directly by the rate, but the apparent frequency factor *A* does. *A* was computed assuming that cracking reactions follow the first-order kinetic law.

The models were computed by using the package of software CHEMKIN II [38], and more 72 precisely SENKIN at constant pressure and temperature. It should be noted that this software 73 uses the ideal gas law to calculate concentrations. Obviously, the ideal gas law is not valid at 74 high pressure either. Consequently, all initial concentrations  $c_0$  were first calculated separately 75 by using the Peng-Robinson equation of state [39] which is implemented in the software 76 DIAGSIM [40]. The Peng-Robinson equation of state has been chosen because it is about two 77 times more precise for the estimation of the densities than the other cubic equations of state as 78 the Soave-Redlich-Kwong equation [41]. The calculation of the densities allows the 79 calculation of the concentrations, and this calculation is performed to evaluate the ideal gas 80 pressures that lead to the same initial concentrations than the Peng-Robinson equation of state 81 computed at 700 bar. Simulation conditions are summarized in Table 1. 82

Simulations were performed and reached up to 30% conversion. The consumption rates rwere computed by CHEMKIN at 30% conversion, and by plotting ln r vs - 1/RT (where R is the ideal gas constant and T the temperature in K) with  $T = T_0$ ,  $T_0 - 2$ ,  $T_0 + 2$ , the slope corresponds to the apparent  $E_a$ . The first-order kinetic law ( $r = k \times c$ , with k the rate constant following the Arrhenius law, k in s<sup>-1</sup> and c in mol.m<sup>-3</sup>) leads to:

88  $ln r = ln A - E_a/RT + ln c$ 

The Y-intercept of the plots ln r vs - 1/RT allows the calculation of A. The results are presented 89 first at laboratory temperature (400°C) and then at geological temperature (200°C). The 90 uncertainty on the computed apparent kinetic parameters depends on: 1) the uncertainty of 91 the intrinsic kinetic parameters of the elementary reactions in the kinetic models, 2) the 92 choices made during the construction of the kinetic model (detailed vs lumped models), 3) the 93 care given to the computations (strict respect of the method, especially iso-conversion), and 94 for A: 4) the precision of the estimation of the initial concentrations. Considering the time and 95 effort given to the calculations, the uncertainty on apparent  $E_a$  is estimated between  $\pm 0.5$ 96 kcal/mol and a factor of 2 for the apparent A. 97

98 99

#### **3.** Kinetic parameters at laboratory temperature (400°C)

100 The hydrocarbons selected for this study are divided into three groups: alkanes (linear and 101 branched), methylaromatics (toluene, methylnaphthalene and trimethylbenzene) and other 102 hydrocarbons, such as naphthenes (methylcyclohexane and butylcyclohexane), decylbenzene 103 and tetralin.

104 *3.1 Alkanes* 

105 The apparent kinetic parameters of alkanes were calculated using the detailed kinetic model of 106 Burklé-Vitzthum et al. [30]. This model was constructed based on a lumping technique, 107 taking into account any linear alkanes between  $C_1$  and  $C_{32}$  as well as model compounds of 108 branched alkanes, as reactants and any crossed reactions, and making up 13 206 free radical 109 reactions. Alkanes with several lengths ranging from  $C_5$  to  $C_{25}$  were studied. Linear alkanes 110 were mostly studied, but the influence of branched structures was investigated by comparing 111  $nC_{15}$  to *iso*C<sub>15</sub>.

Table 2 presents the results at 400°C. It leads to the following comments: 1) kinetic parameters of *n*- and *iso*-alkanes do not exhibit any significant differences due to their similar structure and reactivity, 2) all activation energies are comprised between  $67.0\pm0.5$  and  $69.1\pm0.5$  kcal/mol for any alkane chain length and they increase almost linearly with the chain length (Figure 1), 3) the frequency factor increases with the alkane length.

117 Activation energies obtained from the calculations are similar for any chain length 118 investigated, proving the consistency of the lumping methods results with those of detailed mechanisms. A mean value of 68.5 kcal/mol could be proposed, for every alkane for any
structure and length (n>4).

For  $nC_8$ , the detailed model (91 free radical reactions) of Lannuzel et al. [33] was also tested, and leads to  $A = 6.5 \times 10^{16} \text{ s}^{-1}$  and  $E_a = 67.6$  kcal/mol, as well as the extended model of Bounaceur et al. [26] (182 free radical reactions) which leads to  $A = 6.6 \times 10^{15} \text{ s}^{-1}$  and  $E_a =$ 64.0 kcal/mol. The very simple model of Burklé-Vitzthum et al. [29] in the case of  $nC_{16}$  (13 free radical reactions), which was constructed using a particularly drastic lumping method, leads to  $A = 2.0 \times 10^{15} \text{ s}^{-1}$  and  $E_a = 61.8$  kcal/mol.

The former mechanisms were all constructed and validated at high pressure (700 bar) and
temperatures in the range of 300 - 400°C.

129 Another detailed model [42] was also tested: it was constructed to describe the cracking of  $nC_{12}$  in jet fuel conditions (typically 1 bar and 800°C). In these conditions, short radicals 130 formed via decompositions are predominant, whereas in our conditions (lower temperature 131 and very high pressure), the predominant radicals are those corresponding to the reactant, 132 which are formed via H-transfers [26]. Indeed high pressures favor bimolecular reactions, on 133 the contrary to low pressures that favor unimolecular reactions. Therefore, the free radical 134 reactions, that determine the cracking rates, are different and consequently the apparent 135 kinetic parameters are totally different, even when the mechanism is computed at 400°C and 136 700 bar:  $A = 4.5 \times 10^{13} \text{ s}^{-1}$  and  $E_a = 55.9 \text{ kcal/mol} (A = 1.6 \times 10^{12} \text{ s}^{-1} \text{ and } E_a = 50.4 \text{ kcal/mol} \text{ when}$ 137 the mechanism is computed at P = 1 bar and  $T = 800^{\circ}$ C). This example illustrates the 138 importance of selecting kinetic parameters that are determined in conditions close to those in 139 which they are used. 140

Table 3 gathers the experimental literature data concerning *n*-alkanes in similar *T* and *P* conditions, but the results appear very scattered:  $59 < E_a < 74$  kcal/mol and  $3 \times 10^{13} < A < 7 \times 10^{22}$  s<sup>-1</sup>. The activation energy seems to increase with pressure, but no clear conclusion can be drawn. Agreement is obtained with Béhar and Vandenbroucke [14] and Khorasheh and Gray [20] for nC<sub>16</sub> lumped in a drastic manner, and our results are consistent with those of Song et al. [46] and Zhou and Crynes [45].

147 *3.2 Methylaromatics* 

Three methylaromatics were studied: toluene [32], 1-methylnaphthalene [35] and 1, 3, 5trimethylbenzene [31]. Table 2 gathers the results obtained via computation of the models. The apparent activation energies of the studied methylaromatics are very close, due to their similar structures. The apparent frequency factor of trimethylbenzene is higher than that of toluene due to the reaction path degeneracy.

Literature data concerning several aromatics is presented in Table 3. Some data was found at 153 the same P-T conditions. Concerning toluene, literature activation energies are much higher 154 than those calculated from our mechanisms, but they were determined at higher temperatures 155 and at atmospheric pressure. In these conditions, the cracking mechanisms are different [32]; 156 particularly the bimolecular initiations are negligible while they are of utmost importance at 157 high pressures. Indeed, activation energies of bimolecular initiations are 30 kcal/mol lower 158 159 than unimolecular ones, but they become important only at high pressure and therefore the apparent activation energy is much lower at high pressure than at low pressure. Agreement 160 between experimental [31] and computed activation energy of trimethylbenzene is obtained. 161 Concerning 1-methylnaphthalene, the experimental activation energy [24] is far lower than the 162 163 computed value. The determination of the experimental apparent activation energy requires the determination or the assumption of the kinetic law, which is not needed for the 164 computation of  $E_a$  by our kinetic model using detailed mechanisms (the software CHEMKIN 165 II computes directly the rates according to the reaction mechanisms implied). The 166 determination of the experimental  $E_a$  is generally performed by assuming a first-order law but 167 we demonstrated elsewhere [35] that this assumption is not always true. This may explain the 168 differences between the experimental apparent activation energy and the computed value, 169 especially for methylnaphthalene. 170

#### 171 *3.3 Other hydrocarbons*

Methylcyclohexane [27], butylcyclohexane [34], decylbenzene [28] and tetralin [25] were also studied. The apparent kinetic parameters are in Table 2. The apparent activation energies are in the same order of magnitude at 400°C. Butylcyclohexane appears more reactive than methylcyclohexane. This is due to the cracking of the butyl side chain which is easier than the cracking of the methyl side chain. The literature data concerning naphthenes are presented in Table 3. No literature data was found for methylcyclohexane, but the computed kinetic parameters of butycyclohexane are very close to the experimental ones determined forbutycyclohexane [52, 53] and propylcyclohexane [54].

The computed results of tetralin are far from the values obtained by Yu and Eser [55], 180 although they were determined in neighboring conditions. This difference can be due to the 181 assumption of a first-order kinetic law to determine the experimental value. According to our 182 model, it appears that this assumption is not justified [25]. Another sensitive factor is the 183 amount of impurities [25] (particularly dihydronaphthalene) which greatly influences the 184 reactivity of tetralin and consequently its apparent kinetic parameters. This point is not clearly 185 addressed in the experimental study by Yu and Eser [54] and so the comparison is difficult. In 186 our case, the computations were performed with 0.1% of dihydronaphthalene. The mechanism 187 of 2-ethyltetralin is strongly influenced by the cracking of the side chain and so the 188 189 comparison with tetralin would not be consistent.

190 Concerning long-chain ( $n \ge 4$ ) alkylbenzene in which the long chain allows the retroene 191 reaction [28], no agreement is obtained with the literature data, except with the activation 192 energy of Leigh and Szwarc [50] and the frequency factor of Yu and Eser. These results are 193 surprising but once again, literature data were generally determined at higher temperatures 194 and much lower pressures than in our study, making comparisons quite difficult.

195 *3.4 Relative thermal stability at 400°C* 

To establish a relative scale of stability of the investigated hydrocarbons at 400°C, the conversion X is plotted as a function of temperature T assuming a first-order reaction law (Figure 2). The pyrolysis duration is set to 10 hours, which is a typical duration for pyrolysis in the laboratory. Characteristic S-shaped curves are obtained (Figure 2). The scale of stability between compounds is determined as following: the higher the temperature to reach 50% conversion, the more stable the compound. The following scale is obtained from the least to the most stable compound:

203  $DB < C_{15} < MN < BCH < Tetralin < MCH \approx TMB < toluene$ 

It should be noted that: 1) long alkanes ( $C_{15}$ ) belong to compounds with low stability, 2) cycloalkanes are more stable than  $C_{15}$ , 3) toluene and trimethylbenzene are the most stable compounds and behave very differently from methylnaphthalene and decylbenzene, 4) alkylbenzenes are increasingly reactive as their side chain length increases, 5) the stability ofthe aromatic compounds strongly depends on their structure.

The relative stability of butylcyclohexane and alkanes was studied elsewhere [34] and the relative scale of stability was:

211  $nC_{25} < nC_{16} < nC_{10} \approx BCH < nC_8$ 

212 This is in agreement with our results.

The relative stability of dodecylbenzene, 9-methylphenanthrene and  $nC_{25}$  was evaluated by Béhar et al. (2008), and it should be noted that our results concerning decylbenzene (instead of dodecylbenzene), methylnaphthalene (instead of 9-methylphenanthrene) and  $nC_{15}$  (instead of  $nC_{25}$ ) are in agreement with their results at 400°C.

217

#### 4. Kinetic parameters at geological temperature (200°C)

#### 218 4.1 Alkanes and methylaromatics

Alkanes and methylaromatics kinetic parameters seem to be almost constant between 400°C 219 and 200°C (Table 2) because the free-radical reactions that control the thermal cracking 220 remain the same. The apparent activation energy of alkanes does not depend on the chain 221 length at 200°C on the contrary to 400°C and an average value of 69.3±0.5 kcal/mol can be 222 proposed for any chain length. Nevertheless, the apparent rate constant k increases with the 223 chain length and its evolution can be compared to the correlation of Watanabe et al. [56] 224 validated at 200-700°C and 1-150 bar. Watanabe et al. [56] proposed a correlation that plots 225  $k(nC_i)/k(nC_{16})$  as a function of the chain length i ( $3 \le i \le 32$ ) regardless of the temperature 226 and the pressure. The correlation was validated up to  $i \approx 20$ . We have chosen arbitrarily C<sub>15</sub> as 227 a reference alkane instead of C<sub>16</sub> in this study, so we plotted  $k(nC_i)/k(nC_{15})$  [26, 29, 30, 33] at 228 229 400°C and 200°C as a function of i and we compared it to the correlation established for  $k(nC_i)/k(nC_{16})$  (Figure 3). Agreement with the model [56] was obtained at up to i = 16 for 230 231 both temperatures.

232 *4.2 Other hydrocarbons* 

Table 2 shows that the behavior of decylbenzene and tetralin strongly depends on temperature. In the case of decylbenzene, the previous mechanistic study [28] revealed that the mechanism includes free-radical reactions as well as the molecular retroene reaction. The importance of the retroene reaction increases as temperature decreases because its activation energy (54 kcal/mol) is much lower than the global cracking activation energy of the freeradical (70 kcal/mol). Indeed, at low temperature, the apparent activation energy almost corresponds to the activation energy of the retroene reaction.

The apparent activation energy of tetralin strongly decreases when the temperature decreases but so does the frequency factor. This is due to the bimolecular initiations whose kinetic parameters are much lower than those of unimolecular initiations. So their importance increases when temperature decreases and they strongly influence the apparent kinetic parameters, leading to lower frequency factors and lower activation energies.

245 *4.3 Relative thermal stability at 200°C* 

A relative scale of stability is established at 200°C in the same manner as previously for 400°C, but the duration is set to 100 million years (Figure 4) which is characteristic of geological duration. The apparent kinetic parameters computed at 200°C are used. A different scale of stability is obtained at 200°C (Figure 4) in comparison to 400°C (Figure 2), essentially because the apparent activation energies are different for each compound, but also because of the modification of some kinetic parameters with temperature:

252  $DB < MN < C_{15} \approx TMB < tetralin \approx BCH \approx toluene < MCH$ 

One major difference between both scales of stability is the increase of the relative stability of methylcyclohexane when temperature decreases. Another major difference is the strong increase of the reactivity of decylbenzene with the decrease of temperature due to the retroene reaction as explained above.

The comparison between the relative scales of stability at low and high temperatures appears more difficult for the other compounds. In order to highlight the influence of the modifications of the apparent kinetic parameters, we also computed the relative scale of stability at 200°C, but with the kinetic parameters computed at 400°C, and we obtained:

261  $DB \approx MN < TMB < C_{15} < toluene < BCH \approx MCH \approx tetralin$ 

The major mistake that would be done by using at 200°C the kinetic parameters computed at 400°C, would lie in the overestimation of the stability of tetralin and decylbenzene, in comparison to the other compounds.

#### 265 **5.** Discussion

The apparent kinetic parameters of decylbenzene, methylcyclohexane and tetralin clearly depend on temperature. For all other compounds, the differences between the kinetic parameters computed at 400°C and 200°C could seem negligible. In order to quantify the consequences of these minor changes, we calculated the conversion at 200°C after 1, 10 or 100 million years (depending on the reactivity of the hydrocarbon) by using the apparent kinetic parameters computed at 400°C and 200°C and assuming a first-order law (Table 4). We also calculated the half-life with both apparent kinetic parameters (Figures 5, 6 and 7).

273 *5.1. Alkanes* 

Table 4 and Figure 5 show that simulating at 200°C the apparent kinetic parameters computed at 400°C would lead to a higher reactivity (increase of conversion and decrease of half-life) than using the kinetic parameters computed at 200°C, especially for short alkanes  $(nC_8)$ . The difference is less important when the length of alkanes increases and there is no difference for long alkanes ( $nC_{25}$ ).

279 Differences could be explained by on the weight of decomposition reactions via  $\beta$ -scission of the short radicals among all decomposition reactions. Indeed, the decomposition reactions are 280 rate-limiting at high pressures and low temperatures [26] and they greatly influence the 281 apparent activation energy. The kinetic parameters of the decomposition of short radicals 282 depend more on temperature (higher activation energy) than the kinetic parameters of the 283 other radicals [26]. Moreover, for short alkanes, the weight of decomposition of short radicals 284 among all decomposition reactions is more important than for long-chain alkanes: short 285 radicals are more concentrated during the thermal cracking of short alkanes than of long 286 alkanes. That is why the apparent activation energy of short alkanes depends more on 287 288 temperature than that of long alkanes. As a consequence, the errors made when simulating at 200°C the kinetic parameters determined at 400°C lies on the fact that the alkane studied is 289 290 short.

*5.2. Monoaromatics and naphthenes* 

The computed conversions and half-lives are presented in Table 4, and Figure 6. All these compounds appear to be more stable at 200°C than at 400°C. With the apparent kinetic parameters computed, the conversions are lower while the half-lives higher at 200°C than at

400°C, although the apparent kinetic parameters do not seem to depend on temperature except 295 for methylcyclohexane. In order to evaluate more precisely the temperature-dependence of the 296 apparent first-order kinetic constant k of methylcyclohexane, we computed k(T) in the 297 temperature range of 200-400°C and we plotted k(T) vs 1/RT (R: ideal gas constant and T: 298 temperature) in a logarithmic scale (markers in Figure 8). By considering the apparent kinetic 299 parameters (A and  $E_a$ ) computed at 400°C, we extrapolated the Arrhenius law from 400°C to 300 low temperature and the extrapolated rate constant is referred to k(400). Then we plotted 301 k(400) vs 1/RT (straight lines in a logarithmic scale in Figure 8). It clearly appears that the 302 303 deviation between k(400) and k(T) increases when the temperature decreases and that k(T) < 1304 *k*(400).

#### 305 *5.3. Decylbenzene and tetralin*

The computed conversions and half-lives are presented in Table 4 and Figure 7. Unlike the 306 other hydrocarbons studied, decylbenzene and tetralin appear to be more reactive at 200°C 307 than at 400°C. When the apparent kinetic parameters are computed at 200°C the conversions 308 309 are higher and the half-lives lower than at 400°C. In the case of decylbenzene, as explained 310 above, this increasing reactivity is due to the retroene reaction whose activation energy is particularly low and whose importance increases when the temperature decreases [28]. The 311 312 increasing reactivity of tetralin is probably related to the bimolecular initiations whose importance also increases when the temperature decreases because of their lower activation 313 314 energy than that of unimolecular initiations [25].

The apparent kinetic parameters of decylbenzene and tetralin (Table 2) strongly depend on temperature. In order to evaluate precisely the temperature-dependence of the apparent firstorder kinetic constant k of decylbenzene and tetralin, we computed k(T) in the temperature range of 200-400°C and we plotted ln k(T) vs 1/RT as well as ln k(400) vs 1/RT (Figure 8). It also clearly appears that the deviation between k(400) and k(T) increases when the temperature decreases and that k(T) > k(400).

#### 321 6. Conclusion

In this paper we computed the apparent kinetic parameters (frequency factor A and activation energy  $E_a$ ) of several pure hydrocarbons on the basis of detailed kinetic models previously constructed and validated. The purpose was to evaluate the effects of extrapolating data obtained in a range of temperatures to another. Indeed, thermal cracking reactions take place at 150°C - 200°C for millions of years in geological reservoirs and so all laboratory data are
obtained at about 400°C during some hours or days and then extrapolated.

The calculations were performed at 700 bar and at 400°C and then 200°C. The computation of 328  $E_a$  is independent from the kinetic rate law with our method, but the computation of A is not: 329 we postulated a first-order kinetic law which is of use in the vast majority of geochemistry 330 publications. In the present study, most of the compounds exhibit apparent kinetic parameters 331 that are slightly or even highly different between 400°C and 200°C. Extrapolating apparent 332 kinetic parameters obtained at 400°C, even though they are only slightly different from those 333 at 200°C, can lead to significant differences in terms of half-lives or conversion after several 334 millions of years. All hydrocarbons studied here (alkanes, monoaromatics and naphthenes) 335 appear to be more stable at 200°C than when extrapolating the Arrhenius law from 400°C to 336 337 200°C, except decylbenzene and tetralin which appear much more reactive. To conclude, any extrapolation beyond the original range of temperatures used to determine the apparent kinetic 338 339 parameters has to be considered very carefully, in the geochemistry field, but also in any other application fields of thermal cracking. We previously showed [26] that the same is true for the 340 341 extrapolation beyond the original range of pressure because the importance of bimolecular vs unimolecular reactions can be completely modified. 342

343 To complete the discussion, two more points should be addressed: the choice of the kinetic rate law and the effects of co-reactants. In most studies, a first-order kinetic law is postulated, 344 345 although it clearly appears that this choice is erroneous for some compounds; for instance, the order is close to <sup>1</sup>/<sub>2</sub> for pure alkanes [57] and 2 for pure methylnaphthalene [35]. It would be 346 347 interesting to lead a complete study on the best choice of kinetic order for each hydrocarbon and address the consequences of an erroneous choice on hydrocarbon stability. The second 348 349 point is the effects of co-reactants on the apparent kinetic parameters. We showed on several systems ([29, 33, 58, 59]) that some co-reactants can completely change the stability of 350 hydrocarbons and consequently the apparent kinetic parameters are also very likely to be 351 modified. Therefore, the studies on pure hydrocarbons have a limited range of application. In 352 order to construct bulk kinetic models of mixtures meant to represent oil fractions, a similar 353 study as the one presented here should be performed with binary mixtures: correlations 354 between the apparent kinetic parameters and the content of co-reactants could be obtained and 355 356 then used in bulk kinetic models.

#### 358 **References**

- [1] P. Ungerer, R. Pelet, Extrapolation of the kinetics of oil and gas formation from laboratory
  experiments to sedimentary basins, Nature 327 (1987) 52-54.
- [2] P. Ungerer, F. Béhar, M. Villalba, O.R. Heum, A. Audibert, Kinetic modelling of oil
  cracking, Org. Geochem. 13 (1988) 857-868.
- [3] F. Béhar, S. Kressmann, J.L. Rudkiewicz, M. Vandenbroucke, Experimental simulation in
  a confined system and kinetic modelling of kerogen and oil cracking, Org. Geochem. 19
  (1992) 173–189.
- [4] F. Béhar, Y. Tang, J. Liu, Comparison of rate constants for some molecular tracers
  generated during artificial maturation of kerogens: influence of kerogen type, Org. Geochem.
  26 (1997) 281–287.
- [5] F. Béhar, M. Vandenbroucke, Y. Tang, F. Marquis, J. Espitalié, Thermal cracking of
  kerogen in open and closed systems: determination of kinetic parameters and stoichiometric
  coefficients for oil and gas generation, Org. Geochem. 26 (1997) 321–339.
- [6] F. Béhar, F. Lorant, L. Mazeas, Elaboration of a new compositional kinetic schema for oil
  cracking, Org. Geochem. 39 (2008) 764-782.
- [7] H.J. Schenk, R. Di Primio, B. Horsfield, The conversion of oil into gas in petroleum
  reservoirs. Part 1: Comparative kinetic investigation of gas generation from crude oils of
  lacustrine, marine and fluviodeltaic origin by programmed-temperature closed-system
  pyrolysis, Org. Geochem. 26 (1997) 467–481.
- [8] V. Dieckmann, H.J. Schenk, B. Horsfield, D.H. Welte, Kinetics of petroleum generation
  and cracking by programmed-temperature closed-system pyrolysis of Toarcian Shales, Fuel
  77 (1998) 23-31.
- [9] M.D. Lewan, T.E. Ruble, Comparison of petroleum generation kinetics by isothermal
  hydrous and nonisothermal open-system pyrolysis, Org. Geochem. 33 (2002) 1457-1475.
- 383 [10] M.D. Lewan, M.J. Kotarba, J.B. Curtis, D. Wieclaw, P. Kosakowski, Oil-generation
- 384 kinetics for organic facies with Type-II and -IIS kerogen in the Menilite Shales of the Polish
- 385 Carpathians, Geochim. Cosmochim. Acta 70 (2002) 3351-3368.

- [11] E. Lehne, V. Dieckmann, Bulk kinetic parameters and structural moieties of asphaltenes
  and kerogens from a sulphur-rich source rock sequence and related petroleums, Org.
  Geochem. 38 (1997) 1657-1679.
- [12] E. Lehne, V. Dieckmann, The significance of kinetic parameters and structural markers
  in source rock asphaltenes, reservoir asphaltenes and related source rock kerogens, the
  Duvernay Formation (WCSB), Fuel 86 (2007) 887-901.
- 392 [13] F. Béhar, H. Budzinski, M. Vandenbroucke, Y. Tang, Methane Generation from Oil
- Cracking: Kinetics of 9-Methylphenanthrene Cracking and Comparison with Other Pure
  Compounds and Oil Fractions, Energy Fuels 13 (1999) 471-481.
- 395 [14] F. Béhar, M. Vandenbroucke, Experimental Determination of the Rate Constants of the
- 396 n-C25 Thermal Cracking at 120, 400, and 800 bar: Implications for High-Pressure/High-
- Temperature Prospects, Energy Fuels 10 (1996) 932-940.
- [15] K.J. Jackson, A.K. Burnham, R.L. Braun, K.G. Knauss, Temperature and pressure
  dependence of n-hexadecane cracking, Org. Geochem. 23 (1995) 941–953.
- 400 [16] F. Enguehard, S. Kressmann, F. Dominé, Kinetics of dibutylether pyrolysis at high
  401 pressure experimental study, Org. Geochem. 16 (1990) 155-160.
- 402 [17] F. Béhar, F. Lorant, H. Budzinski, E. Desavis, Thermal Stability of Alkylaromatics in
  403 Natural Systems: Kinetics of Thermal Decomposition of Dodecylbenzene, Energy Fuels 16
  404 (2002) 831-841.
- [18] C. Dartiguelongue, F. Béhar, H. Budzinski, G. Scacchi, P-M. Marquaire, Thermal
  stability of dibenzothiophene in closed system pyrolysis: Experimental study and kinetic
  modeling, Org. Geochem. 37 (2006) 98-116.
- [19] T. Ford, Liquid-Phase Thermal Decomposition of Hexadecane: Reaction Mechanisms,
  Ind Eng. Chem. Fundam. 25 (1986) 240-243.
- [20] F. Khorasheh, M. R. Gray, High-Pressure Thermal Cracking of n-Hexadecane, Ind. Eng.
  Chem. Res. 32 (1993) 1853-1863.
- 412 [21] P.E. Savage, M.T. Klein, Asphaltene Reaction Pathways. 2. Pyrolysis of n413 Pentadecylbenzene, Ind. Eng. Chem. Res. 26 (1987) 488-494.
- 414 [22] P.E. Savage, M.T. Klein, Asphaltene Reaction Pathways. 4. Pyrolysis of
  415 Tridecylcyclohexane and 2-Ethyltetralin, Ind. Eng. Chem. Res. 27 (1988) 1348-1356.

- 416 [23] P.E. Savage, K.L. Baxter, Pathways, Kinetics, and Mechanisms for 2-Dodecyl-9,10417 dihydrophenanthrene Pyrolysis, Ind. Eng. Chem. Res. 35 (1996) 1517-1523.
- [24] J-P. Leininger, F. Lorant, C. Minot, F. Béhar, Mechanisms of 1-methylnaphthalene
  pyrolysis in a batch reactor, Energy Fuels 20 (2006) 2518-2530.
- 420 [25] R. Bounaceur, G. Scacchi, P-M. Marquaire, F. Dominé, Mechanistic modeling of the
  421 thermal cracking of tetralin, Ind. Eng. Chem. Res. 39 (2000) 4152-4165.
- 422 [26] R. Bounaceur, F. Lannuzel, R. Michels, G. Scacchi, P-M. Marquaire, V. Burklé-
- 423 Vitzthum, Influence of pressure (100 Pa-100 MPa) on the pyrolysis of an alkane at moderate
- 424 temperature (603K-723 K): Experiment and kinetic modeling, J. Anal. Appl. Pyrolysis 122
- 425 (2016) 442-451.
- 426 [27] R. Bounaceur, V. Burklé-Vitzthum, P-M. Marquaire, L. Fusetti, Mechanistic modeling of
- 427 the thermal cracking of methylcyclohexane near atmospheric pressure, from 250 to 1000°C,
- 428 Identification of aromatization pathways, J. Anal. Appl. Pyrolysis 103 (2013) 240-254.
- 429 [28] V. Burklé-Vitzthum, R. Michels, G. Scacchi, P-M. Marquaire, Mechanistic Modeling of
- 430 the Thermal Cracking of Decylbenzene, Ind. Eng. Chem. Res. 23 (2003) 5791-5808.
- 431 [29] V. Burklé-Vitzthum, R. Michels, G. Scacchi, P-M. Marquaire, D. Dessort, B. Pradier, O.
- Brevart, Kinetic Effect of Alkylaromatics on the Thermal Stability of Hydrocarbons under
  Geological Temperatures, Org. Geochem. 35 (2004) 3-31.
- 434 [30] V. Burklé-Vitzthum, R. Bounaceur, P-M. Marquaire, F. Montel, L. Fusetti, Thermal
  435 evolution of n- and iso-alkanes in oils. Part 1: Pyrolysis model for a mixture of 78 alkanes
  436 (C1-C32) including 13,206 free radical reactions, Org. Geochem. 42 (2011) 439-450.
- [31] L. Fusetti, F. Béhar, R. Bounaceur, P-M. Marquaire, K. Grice, S. Derenne, New insights
  into secondary gas generation from the thermal cracking of oil: Methylated aromatics. A
  kinetic approach using 1,2,4-trimethylbenzene. Part I: A mechanistic model, Org. Geochem.
  41 (2010) 146-167.
- [32] F. Lannuzel, R. Bounaceur, R. Michels, G. Scacchi, P-M. Marquaire, An extended
  mechanism including high pressure conditions (700 bar) for toluene pyrolysis, J. Anal. Appl.
  Pyrolysis 87 (2010) 236-247.
- 444 [33] F. Lannuzel, R. Bounaceur, R. Michels, G. Scacchi, P-M. Marquaire, Reassessment of
- the kinetic influence of toluene on *n*-alkane pyrolysis, Energy Fuels 24 (2010) 3817-3830.

- [34] D. Rakatoalimanana, F. Béhar, R. Bounaceur, V. Burkle-Vitzthum, P-M. Marquaire,
  Thermal cracking of n-butylcyclohexane at high pressure (100 bar) part 2: mechanistic
  modeling, J. Anal. Appl. Pyrolysis, 120 (2016) 174-185.
- 449 [35] R. Bounaceur, J.F. Leininger, F. Lorant, P-M. Marquaire, V. Burklé-Vitzthum, Kinetic
- 450 modeling of 1-Methylnaphthalene pyrolysis at high pressure (100 bar), J. Anal. Appl.
- 451 Pyrolysis (2017) accepted JAAP3952.
- 452 [36] F. Dominé, P.M. Marquaire, C. Muller, G.M. Côme, Kinetics of hexane pyrolysis at very
- 453 high pressures. 2. Computer modeling, Energy Fuels 4 (1990) 2-10.
- 454 [37] F. Dominé, R. Bounaceur, G. Scacchi, P.M. Marquaire, D. Dessort, B. Pradier, O.
- 455 Brevart, Up to what temperature is petroleum stable? New insights from a 5200 free radical 456 reactions model, Org. Geochem. 33 (2002) 1487–1499.
- 457 [38] R.J. Kee, F.M. Rupley, J.A. Miller, Chemkin-II: A Fortran chemical kinetics package for
- the analysis of gas-phase chemical kinetics. Sandia National Laboratories, Livermore, CA,1989.
- [39] D.-Y Peng, D. B. Robinson, A new two-constant equation of state, Ind. Eng. Chem.
  Fundam. 15 (1976) 59-64.
- [40] J-N. Jaubert, Présentation du logiciel DiagSim permettant de faciliter l'enseignement de
  la thermodynamique technique, International Journal of Technologies in Higher Education 2
  (2005) 34-47.
- [41] R. Privat, M. Visconte, A. Zazoua-Khames, J-N. Jaubert, R. Gani, Analysis and
  prediction of the alpha-function parameters used in cubic equations of state, Chem. Eng. Sc.
  126 (2015) 584-603.
- [42] O. Herbinet, P-M. Marquaire, F. Battin-Leclerc, R. Fournet, Thermal stability of ndodecane: experiments and kinetic modeling, J. Anal. Appl. Pyrolysis 78 (2007) 419-429.
- [43] D. Kunzru, Y. T. Shah, E. B. Stuart, Thermal Cracking of n-Nonane, Ind. Eng. Chem.
  Process Des. Dev. 11 (1972) 605-612.
- 472 [44] J. Yu, S. Eser, Kinetics of Supercritical-Phase Thermal Decomposition of C10-C14
- 473 Normal Alkanes and Their Mixtures, Ind. Eng. Chem. Res. 36 (1997) 585-591.

- 474 [45] P. Zhou, B.L. Crynes, Thermolytic Reactions of Dodecane. Ind.Eng. Chem. Process Des.
  475 Dev. 25 (1986) 508-514.
- 476 [46] C. Song, W.C. Lai, H.H. Schobert, Condensed-Phase Pyrolysis of n-Tetradecane at
- 477 Elevated Pressures for Long Duration. Product Distribution and Reaction Mechanisms, Ind.
- 478 Eng. Chem. Res. 33 (1994) 534-547.
- 479 [47] B. Blouri, F. Hamdan, D. Herault, Mild Cracking of High-Molecular-Weight
  480 Hydrocarbons, Ind. Eng. Chem. Process Des. Dev. 24 (1985) 30-37.
- [48] S.B. Domke, R.F. Pogue, F.J.R. Van Neer, C.M. Smith, Investigation of the kinetics of
  ethylbenzene pyrolysis using a temperature-scanning reactor, Ind. Eng. Chem. Res. 40 (2001)
  5878-5884.
- 484 [49] W.D. Clark, S.P. Price, Free-radical and MolecularProcesses in the Pyrolysis of
  485 Ethylbenzene, Can. J. Chem. 48 (1970) 1059.
- [50] C.H. Leigh, M. Szwarc, The pyrolysis of normal-butylbenzene and the heat of formation
  of normal-propyl radical, J. Chem. Phys. 20 (1952) 407-411.
- [51] H. Freund, W.N. Olmstead, Detailed chemical kinetic modeling of butylbenzene
  pyrolysis, Int. J. Chem. Kinet. 21 (1989) 561-574.
- 490 [52] J. Yu, S. Eser, Thermal Decomposition of Jet Fuel Model Compounds under Near491 Critical and Supercritical Conditions. 1. n-Butylbenzene and n-Butylcyclohexane, Ind. Eng.
  492 Chem. Res. 37 (1998) 4591-4600.
- [53] D. Rakatoalimanana, F. Béhar, R. Bounaceur, V. Burklé-Vitzthum, P-M. Marquaire,
  Thermal cracking of n-butylcyclohexane at high pressure (100 bar) part 1: experimental
  study, J. Anal. Appl. Pyrolysis, 117 (2016) 1-16.
- 496 [54] J. A. Widegren, T. J. Thomas, Thermal decomposition kinetics of kerosene-based rocket
  497 propellants. 1. Comparison of RP-1 and RP-2, Energy Fuels 23 (2009) 5517-5522.
- [55] J. Yu, S. Eser, Thermal Decomposition of Jet Fuel Model Compounds under NearCritical and Supercritical Conditions. 2. Decalin and Tetralin, Ind. Eng. Chem. Res. 37 (1998)
  4601-4608.

- [56] M. Watanabe, T. Adschiri, K. Arai, Overall Rate Constant of Pyrolysis of n-Alkanes at a
  Low Conversion Level, Ind. Eng. Chem. Res. 40 (2001) 2027-2036.
- 503 [57] R. Bounaceur, Modélisation cinétique de l'évolution thermique des pétroles dans les
  504 gisements, PhD Thesis, INPL Nancy France, 2001.
- 505 [58] V. Burklé-Vitzthum, R. Michels, R. Bounaceur, P-M. Marquaire, G. Scacchi,
  506 Experimental study and modelling of the role of hydronaphthalenics on the thermal stability
  507 of hydrocarbons under laboratory and geological conditions, Ind. Eng. Chem. Res. 44 (2005)
  508 8972-8987.
- [59] R. Bounaceur, G. Scacchi, P-M. Marquaire, F. Dominé, O. Brévart, D. Dessort, B.
  Pradier, Inhibiting effect of tetralin on the pyrolysic decomposition of hexadecane.
  Comparison with toluene, Ind. Eng. Chem. Res. 41 (2002) 4689-4701.
- 512

# 513 List of tables

	Initial	Ideal gas pressure	Initial	Ideal gas pressure
	concentration	(bar) equivalent to	concentration	(bar) equivalent to
	(mol/m <sup>3</sup> )	700 bar at 400°C	(mol/m <sup>3</sup> )	700 bar at 200°C
	700 bar - 400°C		700 bar - 200°C	
<i>n</i> C <sub>5</sub> H <sub>12</sub>	6948	389	8319	327
nC <sub>6</sub> H <sub>14</sub>	6280	351	7330	288
<i>n</i> C <sub>8</sub> H <sub>18</sub>	5208	291	5878	231
nC <sub>12</sub> H <sub>26</sub>	3602	202	3903	153
nC14H30	3038	170	3250	128
<i>n-</i> or <i>iso</i>	2797	156	2976	117
C15H32				
<i>n</i> C <sub>16</sub> H <sub>34</sub>	2579	144	2731	107
<i>n</i> C <sub>25</sub> H <sub>52</sub>	1376	77	1420	56
Toluene	7470	418	8700	342
1-Methyl- naphtalene	5919	331	6494	255
Trimethyl-benzene	6002	336	6756	266
Decylbenzene	3080	172	3281	129
Tetralin	5793	324	6404	252
Methyl- cyclohexane	6526	365	7486	294
Butylcyclohexane	4744	265	5223	205

Table 1: Simulation conditions deduced from Peng Robinson equation of state.

# 521 Table 2: Computed apparent kinetic parameters.

## 

Hydrocarbons	A (s <sup>-1</sup> )	$E_a$ (kcal/mol)	A (s <sup>-1</sup> )	$E_a$ (kcal/mol)
	400°C		200°C	
<i>n</i> C <sub>5</sub> H <sub>12</sub> [30]	$1.1 \times 10^{16}$	67.2	5.3× 10 <sup>16</sup>	69.2
<i>n</i> C <sub>6</sub> H <sub>14</sub> [30]	3.6× 10 <sup>16</sup>	67.3	1.6× 10 <sup>17</sup>	69.3
<i>n</i> C <sub>8</sub> H <sub>18</sub> [30]	$7.7 \times 10^{16}$	67.0	$1.8 \times 10^{17}$	69.2
<i>n</i> C <sub>8</sub> H <sub>18</sub> [26]	6.6× 10 <sup>15</sup>	64.0	$1.7 \times 10^{18}$	71.8
<i>n</i> C <sub>8</sub> H <sub>18</sub> [33]	$6.5 \times 10^{16}$	67.6		
<i>n</i> C <sub>12</sub> H <sub>26</sub> [30]	$1.8 \times 10^{17}$	68.6	2.2× 10 <sup>17</sup>	69.3
<i>n</i> C <sub>14</sub> H <sub>30</sub> [30]	1.6× 10 <sup>17</sup>	68.2	$3.0 \times 10^{17}$	69.2
<i>n</i> C <sub>15</sub> H <sub>32</sub> [30]	1.8× 10 <sup>17</sup>	67.8	5.2× 10 <sup>17</sup>	69.3
<i>iso</i> C <sub>15</sub> H <sub>32</sub> [30]	$1.7 \times 10^{17}$	67.9	5.3× 10 <sup>17</sup>	69.3
<i>n</i> C <sub>16</sub> H <sub>34</sub> [29]	2.0× 10 <sup>15</sup>	61.8		
<i>n</i> C <sub>25</sub> H <sub>52</sub> [30]	6.5× 10 <sup>17</sup>	69.1	$7.3 \times 10^{17}$	69.2
Toluene	$2.9 \times 10^{10}$	54.4	$4.0 \times 10^{10}$	55.4
1-Methylnaphtalene	$1.3 \times 10^{14}$	59.3	$1.8 \times 10^{14}$	60.2
Trimethylbenzene	8.8× 10 <sup>11</sup>	56.1	1.4× 10 <sup>12</sup>	57.3
Decylbenzene	$1.2 \times 10^{18}$	67.0	$4.9 \times 10^{12}$	54.0
Tetralin	7.4× 10 <sup>15</sup>	67.5	2.6× 10 <sup>13</sup>	61.2
Methylcyclohexane	$1.9 \times 10^{14}$	63.7	$1.5 \times 10^{15}$	66.4
Butylcyclohexane	$4.7 \times 10^{16}$	68.4	7.6×10 <sup>16</sup>	69.4

## 527 Table 3: Literature data.

Compound	E (kcal/mol)	A (s <sup>-1</sup> )	Ref.	T-P conditions
<i>n</i> C9H20	63	2.0×10 <sup>14</sup>	Kunzru et al., [42]	650-750°C
<i>n</i> C10H22	60	3.6×10 <sup>21</sup>	Yu and Eser, [43]	400-450°C 21 bar
<i>n</i> C <sub>12</sub> H <sub>26</sub>	62	2.3×10 <sup>22</sup>	Yu and Eser, [43]	400-450°C 18 bar
<i>n</i> C12H26	65.2	3.7×10 <sup>16</sup>	Zhou and Crynes, [44]	250-440°C 92-103 bar
<i>n</i> C14H30	63	7.2×10 <sup>22</sup>	Yu and Eser, [43]	400-450°C 16 bar
<i>n</i> C14H30	67.6	7.2×10 <sup>18</sup>	Song et al., [45]	450°C 20-90 bar
<i>n</i> C <sub>16</sub> H <sub>34</sub>	59.2	3.1×10 <sup>13</sup>	Blouri et al., [46]	350-440°C 20 bar
<i>n</i> C16H34	59.6	3.1×10 <sup>14</sup>	Ford, [19]	330-420°C Liquid phase
<i>n</i> C <sub>16</sub> H <sub>34</sub>	61.2	1.5×10 <sup>15</sup>	Khorasheh and Gray, [20]	380-450°C 139 bar
<i>n</i> C <sub>16</sub> H <sub>34</sub>	74	3.0×10 <sup>19</sup>	Jackson et al., [15]	300-370°C 150-600 bar
<i>n</i> C <sub>25</sub> H <sub>52</sub>	68.2	6.1×10 <sup>17</sup>	Behar and Vandenbroucke, [14]	325-425°C 120-800 bar

Toluene	66.0	3.3×10 <sup>13</sup>	Domke et al.,	540-700°C
			[47]	1 bar
Toluene	70.1	4.8×10 <sup>14</sup>	Clark and Price, [48]	?
1-methylnaphthalene	47.4	7.9×10 <sup>9</sup>	Leininger et al., [24]	380-450°C 100 bar
Trimethylbenzene	58.0	1.1×10 <sup>12</sup>	Fusetti et al., [31]	395-475°C 100 bar
Ethylbenzene	62.3	4.7×10 <sup>13</sup>	Domke et al., [47]	540-700°C 1 bar
Butylbenzene	65	3.0×10 <sup>14</sup>	Leigh and Szwarc, [49]	?
Butylbenzene	52.9	1.1×10 <sup>12</sup>	Freund and Olmstead, [50]	505-650°C
Butylbenzene	57	4.0×10 <sup>17</sup>	Yu and Eser, [51]	400-450°C 20-85 bar
Dodecylbenzene	53.3	1.3×10 <sup>13</sup>	Behar et al., [17]	325-425°C 140 bar
Pentadecylbenzene	55.5	1.1×10 <sup>14</sup>	Savage and Klein, [21]	375-450°C 1-9.7 bar
9- Methylphenanthrene	49.0	4.5×10 <sup>10</sup>	Behar et al., [13]	375-450°C 120 bar
Dibenzothiophene	59.0	1.9×10 <sup>11</sup>	Dartiguelongue et al., [18]	375-500°C 100 bar
2-Dodecyl-9,10- dihydrophenanthrene	54.5 ± 9.1	4.0×10 <sup>13</sup>	Savage and Baxter, [23]	375-450°C
Tetralin	58.0	3.5×10 <sup>12</sup>	Yu and Eser, 1998	425-475°C

					23-75 bar
	2-Ethyltetralin	53.5	5.0×10 <sup>12</sup>	Savage and Klein, 1988	375-450°C
	Propylcyclohexane	67.6	2.6×10 <sup>16</sup>	Widegren and Bruno, [53]	350-450°C 3500 bar
	Butylcyclohexane	65.0	3.5×10 <sup>15</sup>	Yu and Eser, [54]	425-475°C 17-86 bar
	Butylcyclohexane	69.0	6.7×10 <sup>16</sup>	Rakatoalimanana et al., [52]	300-425°C 100 bar
529					I
530					
531					
532					
533					
534					
535					
536					
537					
538					
539					
540					
541					
542					
543					

- Table 4: Temperature-dependence of kinetic parameters of some hydrocarbons: influence on
- 545 conversion at 200°C.
- 546

	<i>n</i> C <sub>8</sub> H <sub>18</sub>		<i>n</i> C <sub>15</sub> H <sub>32</sub>		
	First-order law	First-order law	First-order law	First-order law	
	using A and Ea	using A and Ea	using A and Ea	using A and Ea	
	calculated at	calculated at	calculated at	calculated at	
	400°C	200°C	400°C	200°C	
<b>Conversion after</b>	91%	45%	93%	78%	
10 million years					
	nC <sub>2</sub>	5H52	Tolu	uene	
	First-order law	First-order law	First-order law	First-order law	
	using A and Ea	using A and Ea	using A and Ea	using A and Ea	
	calculated at	calculated at	calculated at	calculated at	
	400°C	200°C	400°C	200°C	
<b>Conversion after</b>	91%	91%	49%	27%	
10 million years					
	1-Methylnaphtalene		Trimethylbenzene		
	First-order law	First-order law	First-order law	First-order law	
	using A and Ea	using A and Ea	using A and Ea	using A and Ea	
	calculated at	calculated at	calculated at	calculated at	
	400°C	200°C	400°C	200°C	
<b>Conversion after</b>	100%	100%	96%	77%	
10 million years					
	D	DB		Tetralin	
	First-order law	First-order law	First-order law	First-order law	
	using A and Ea	using A and Ea	using A and Ea	using A and Ea	
	calculated at	calculated at	calculated at	calculated at	
	400°C	200°C	400°C	200°C	
<b>Conversion after</b>	100% (98% after	100% (100% after	78%	99%	
100 million years	1 million years)	1 million years)			
	M	МСН		CH	
	First-order law	First-order law	First-order law	First-order law	
	using A and Ea	using A and Ea	using A and Ea	using A and Ea	
	calculated at	calculated at	calculated at	calculated at	

	400°C	200°C	400°C	200°C
Conversion after 100 million years	89%	63%	97%	87%

## **Figure captions**

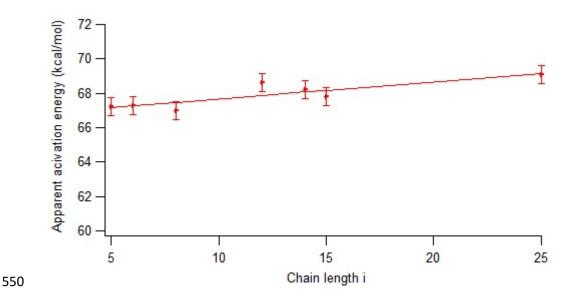


Figure 1: Apparent activation energy computed at 400°C as a function of the chain length *i* (linear regression:  $E_a$  (*kcal/mol*) = 0.10×*i* + 66.7).

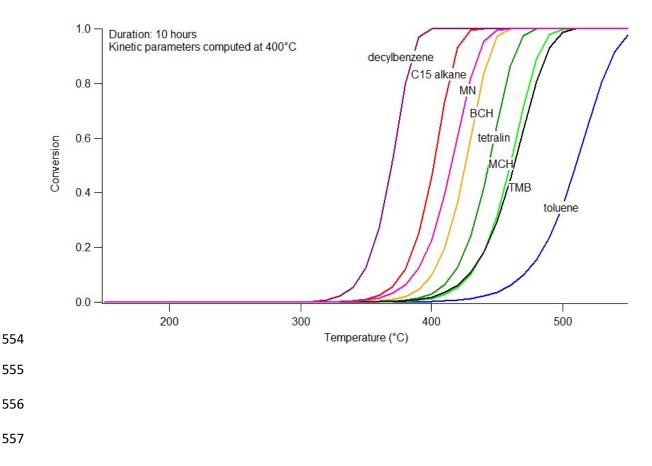
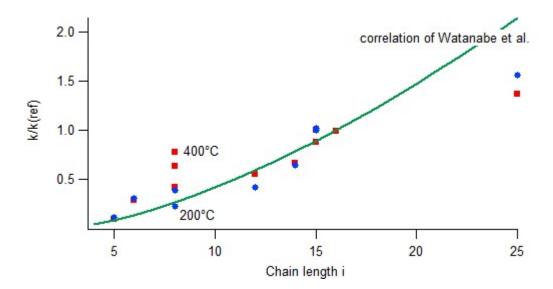
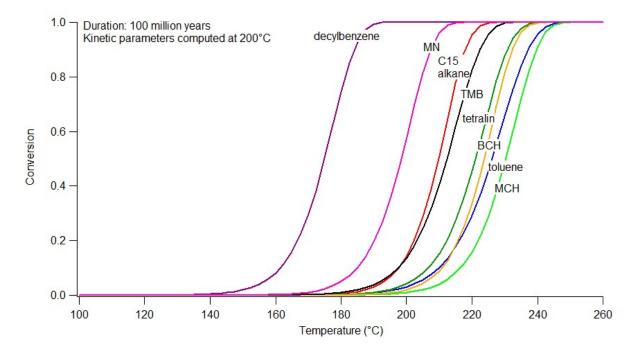


Figure 2: Relative stability of the hydrocarbons determined by using the apparent kinetic
parameters calculated at 400°C (pyrolysis duration set to 10 h).



562

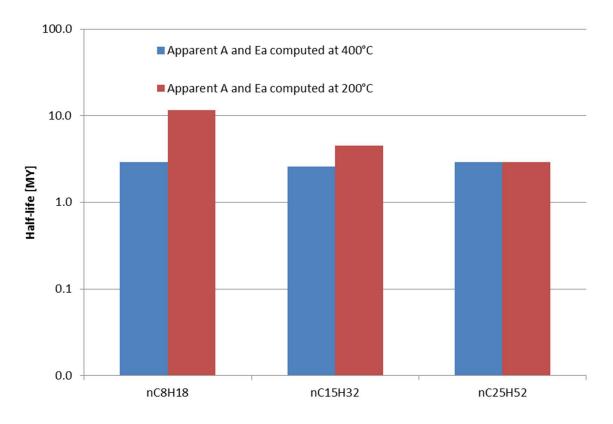
Figure 3: Comparison of the normalized rate constants [26, 29, 30, 33] (C<sub>15</sub> as the reference
compound) as a function of the chain length to the correlation of Watanabe et al. [55] (square
markers: 400°C and circle markers: 200°C).



566

567 Figure 4: Relative stability of the hydrocarbons determined by using the apparent kinetic 568 parameters calculated at 200°C (pyrolysis duration set to 100 million years).

569



571

572 Figure 5: Temperature-dependence of kinetic parameters of some alkanes: influence on half-

573 life at 200°C.

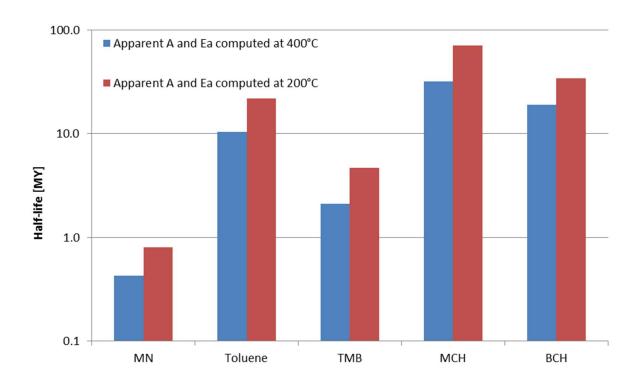
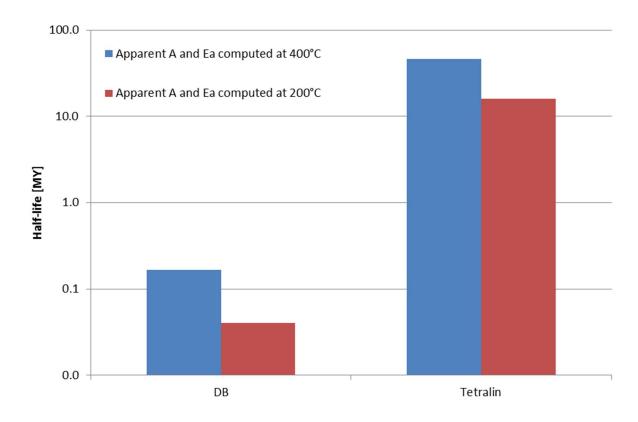


Figure 6: Temperature-dependence of kinetic parameters of methylaromatics and naphthenes:influence on half-life at 200°C.



577

Figure 7: Temperature-dependence of kinetic parameters of decylbenzene and tetralin:influence on half-life at 200°C.

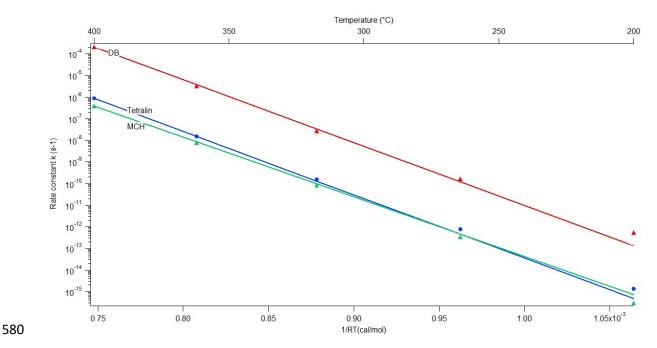


Figure 8: Computed evolution of the rate constants (decylbenzene, methylcyclohexane and tetralin) as a function of temperature compared with the extrapolation of the Arrhenius law from 400°C.