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1         **Ab initio screening of zeolite Y formulations for efficient adsorption of**  
2                                   **thiophene in presence of benzene**

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16 **ABSTRACT**

17

18 In the context of deep desulfurization of transport fuels, the present work aimed at identifying  
19 a suitable material for the selective removal of thiophene from fuels. Dispersion corrected  
20 density functional theory (DFT) calculations have been carried out in order to investigate the  
21 adsorption of benzene and thiophene in various faujasite zeolite formulations including DAY,  
22 HY, LiY, NaY, KY, CsY, Cu(I)Y, Cu(II)Y, Ag(I)Y, Zn(II)Y, and FAU containing Lewis acid  
23 sites (LAS) (defect or extra-framework). Bearing-LAS FAU, Cu(I)Y, Cu(II)Y, Zn(II)Y, CsY,  
24 and HY showed a higher affinity towards thiophene adsorption. In particular, thiophene is  
25 more adsorbed on defect LAS than benzene by 17.7 kJ/mol, suggesting that this zeolite could  
26 be chosen as a suitable candidate for the optimal selective adsorption of thiophene in the  
27 presence of benzene. In terms of regenerability, all formulations can be safely used (except  
28 the one containing extra-framework Lewis acid sites) as they can limit the activation of the C-  
29 S bond of thiophene. Considering both adsorption selectivity and sorbent regenerability  
30 criteria, faujasites containing defect Lewis acid sites could be chosen as a good compromise  
31 to perform a selective adsorption of thiophene in presence of benzene.

32 **Keywords:** Desulfurization, porous, cation, faujasite, DFT, sulfur

33

## 1. Introduction

The environmental legislation of many countries requires a reduction of the sulfur contents of gasoline and diesel fuels from 400-500 to 0.1-0.2 ppm [1–3], since sulfur-bearing compounds present in commercial fuels contribute to catalyst poisoning during petroleum refining, and to toxic SO<sub>x</sub> emissions during fuel combustion in vehicles [4,5]. Thus, deep desulfurization of transport fuels is currently a major world research topic [6–9]. Several efficient technologies already exist such as hydrodesulfurization (HDS) [10,11], extractive desulfurization (EDS) [12], reactive adsorption desulfurization (RADS) [13], oxidative desulfurization (ODS) [14], and adsorptive desulfurization (ADS) [15]. Sulfur compounds are present in fuels as thiols, thioethers and thiophenic species. HDS appears as an efficient technology for thiol and thioether removal, but the process is inefficient for the elimination of thiophenic compounds such as 4,6-dimethyldibenzothiophene which is the most refractory compound to HDS [16]. Moreover, HDS can generate H<sub>2</sub>S, which is inhibitory for the deep hydrodesulfurization of the most refractory compounds [17]. Adsorption desulfurization (ADS) can be considered as one of the most promising processes to ultra-clean diesel and gasoline under moderate conditions (ambient temperature and atmospheric pressure) [4,8,15,16,18–21]. Its success is due to the development of highly selective sorbents showing a higher affinity for sulfur compounds than for other major fuel components, and to other criteria such as an excellent adsorption capacity and good sorbent reusability [20–25]. However, the adsorption of sulfur species on sorbents undergoes a strong competition on the adsorption sites with desired aromatics, such as benzene. Commercially available sorbents tested are zeolites, activated charcoal, and activated alumina [26–31]. The zeolite ZSM-5 was shown to be more selective for thiophene than for benzene, toluene, and p-xylene [32]. However, its limited pore size (5.2 to 5.6 Å [33]) sterically hinders or excludes the adsorption of bulky sulfur compounds presenting more than one aromatic ring. Faujasite type zeolites (FAU) which have larger pore sizes and

60 volumes should be more suitable than ZSM-5 for the adsorption of aromatic sulfur  
61 compounds. They present a large supercage of 11.0 x 13.0 Å with a large pore opening of 7.4  
62 x 7.4 Å, numerous adsorption sites in the supercages, and excellent thermal stability [6,8,34–  
63 37].

64 To be selected for ADS technology, sorbents need to combine both high selectivity and good  
65 regeneration ability. These two criteria can be estimated by determining the sorbent affinity  
66 for various desirable and undesirable molecules present in fuels. Using molecular orbital  
67 (MO), Yang et al. [38] investigated  $\pi$ -complexation between thiophene/benzene and transition  
68 metals. They also explored the selectivity and reversibility of  $\pi$ -complexation. However, the  
69 interactions between thiophene and transition metals are governed by  $\pi$ -complexation, which  
70 makes its separation from aromatic hydrocarbons too difficult. Moreover, numerous studies  
71 have shown a strong competition between aromatic and thiophenic compounds [17,19,28] for  
72 adsorption on various sorbents such as H-ZSM5, H-Beta, HY, AgY, CuY, NaY, H-USY, Na-  
73 ZSM-5, activated carbon, and modified activated alumina. Experimental studies have  
74 demonstrated that benzene [8] and toluene [39,40] inhibit the adsorption of thiophene in HY  
75 zeolites. Using nine types of zeolites, including FAU, FER, and MFI, Zeng et al. [17]  
76 investigated the selective adsorption of thiophene in the presence of benzene as a model for  
77 aromatic molecules, and showed a strong competition between benzene and thiophene. In  
78 fact, in binary mixtures, the sorbent selectivity for thiophene highly depends on pore size,  
79 with the optimum pore diameter being between 4.6 and 5.0 Å. In the same context, Duan et al.  
80 [18] showed that the efficiency of sulfur compounds removal decreased in the presence of  
81 benzene and o-xylene. Using several sorbents including Ag-Y, Cu-Y, Na-Y, H-USY, Na-  
82 ZSM-5, activated carbon, and modified activated carbon, Takahashi et al. [28] experimentally  
83 investigated benzene/thiophene adsorption. They reported excellent adsorption performances

84 in terms of adsorption and separation capacity for Cu-Y and Ag-Y. However, these results  
85 were given without molecular explanations.

86 Density Functional Theory (DFT) calculations have been widely used for identifying suitable  
87 zeolite formulations for selective trapping applications such as phenol separation from toluene  
88 for the purification of biofuels [34,41–44], trapping of iodine species released during nuclear  
89 incidents [45–47], and the separation of NO<sub>x</sub> and CO from H<sub>2</sub>O and CO<sub>2</sub> for the prevention of  
90 harmful emissions from diesel engines in confined spaces [48].

91 The present work aims at providing new insights into the capture of thiophene by FAU type  
92 zeolites in the presence of benzene, using dispersion corrected periodic DFT calculations,  
93 with taking in account van der Waals (vdW) interactions. More precisely, our objectives are  
94 to highlight the influence of the compensating charge cation of the zeolite for thiophene  
95 adsorption, and to identify the most efficient FAU formulation, in terms of selectivity and  
96 regenerability, for thiophene adsorption in the presence of benzene. Selected formulations are  
97 as follows: DAY (Si/Al=∞), D-LAS (Defect Lewis acid site of a Faujasite) [41], EX LAS  
98 (Extra-framework Lewis acid site) [41], and the cationic forms HY, LiY, NaY, KY, CsY,  
99 Cu(I)Y, Ag(I)Y, Zn(II)Y, Cu(II)Y (Si/Al ratio of 2.43). To our knowledge, there is no DFT  
100 investigation dedicated to this issue.

101 The present paper is organized as follows: the first part describes in details our  
102 computational procedure; the second part presents and discusses the obtained results, with  
103 focusing on the potential inhibitory effect of benzene on thiophene adsorption; finally, the  
104 third and last part outlines the main conclusions of the present work.

105

## 106 **2. Computational details**

107

### 108 *2.1 Methods*

109

110 Thiophene and benzene adsorption onto FAU zeolites were investigated using the Vienna Ab-  
111 initio Simulation Package (VASP) [49]. For these tasks, our DFT calculations employed the  
112 PBE functional and projector augmented plane wave (PAW) method [50,51] with a chosen  
113 plane wave cutoff energy of 450 eV. Kohn-Sham equations were solved iteratively until the  
114 energy difference between cycles became lower than  $10^{-6}$  eV, while the Gaussian smearing  
115 was fixed to 0.1 eV. Sampling of the Brillouin zone was limited to the  $\Gamma$ -point. FAU  
116 structures were entirely optimized until all the forces fall below 0.01 eV/Å per atom. In order  
117 to account for the vdW interactions, the PBE+TS/HI level of theory [52,53] was used. This  
118 method has been proven to describe accurately ionic systems such as cationic zeolites  
119 [41,48,54]. Adsorption phenomena were evaluated with determining the interaction energy  
120  $\Delta E_{\text{int}}$  between a molecule and a FAU formulation, as indicated in our previous works [54–59].

121

## 122 *2.2 Structural model*

123 The FAU structure is made up of cuboctahedron sodalite units connected to each other by  
124 hexagonal prisms (D6R), leading to the formation of large empty cavities well known as  
125 supercages. Interconnections between supercages and their hexagonal windows (6MR) form  
126 the porosity of the FAU structures. The pure siliceous structure (DAY) is crystallized within  
127 the Fd3m symmetry space group [60] and its supercell structure has the lattice parameters of  
128  $a=b=c = 25.028 \text{ \AA}$  (576 atoms, Si<sub>192</sub>O<sub>384</sub>) and  $\alpha = \beta = \gamma = 90^\circ$  [61]. By means of the DFT  
129 approach, it is difficult in terms of current computational efforts to study the FAU supercell.  
130 Therefore, primitive rhombohedral FAU have been used, containing only 144 atoms and  
131 represented by two supercages and eight hexagonal windows connecting sodalite cages with  
132 supercages, in line with previous studies [62–64]. Twelve FAU structures have been  
133 investigated, namely DAY, cation exchange faujasites MY (Si/Al=2.43), where M= H, Li,  
134 Na, K, Cs, Cu (I), Ag (I), Zn (II), Cu (II), D-LAS and EX-LAS. DAY is a pure siliceous

135 structure with a Si/Al ratio of  $\infty$  exhibiting a high hydrophobicity [65]. D-LAS is modeled by  
136 an excess of negative charge around the placement of the atoms of  $\text{AlO}_4$  in FAU (Si/Al = 47;  
137 resulting from a simple substitution of  $\text{Si}^{4+}$  by  $\text{Al}^{3+}$ ) [41,66], while EX-LAS is represented by  
138 the substitution of the three  $\text{Si}^{4+}$  by three  $\text{Al}^{3+}$  in a 6MR window, and the addition of an extra  
139 framework  $\text{Al}^{3+}$  cation in order to achieve total neutrality in FAU [41].

140

### 141 **3. Results and discussion**

#### 142 *3.1. Adsorption of benzene and thiophene in FAU zeolites*

143  
144 The present part provides a systematic DFT investigation of thiophene and benzene  
145 adsorption on the following FAU formulations: DAY, D-LAS and EX-LAS Lewis acid site  
146 models, and MY (where M= H, Li, Na, K, Cs, Cu (I), Ag (I), Zn (II), Cu (II)). Calculations  
147 were performed using the TS/HI level of theory (PBE+TS/HI). Adsorption configurations are  
148 reported in Table S1 (supporting information) and Fig. 1, while total interaction energies are  
149 shown in Table 1 and Fig. 2.

##### 150 *3.1.1. Adsorption of thiophene*

151 In DAY, both the sulfur atom and the aromatic ring contribute together to the adsorption of  
152 thiophene with  $\Delta E_{\text{int}}$  of 41.5 kJ/mol. This adsorption is controlled by the interactions of the  
153 center of a 6MR window of DAY with carbon atoms in thiophene at distances of 3.70-3.94 Å,  
154 and with the sulfur atom at a distance of 4.21 Å. For any other FAU formulation,  $\Delta E_{\text{int}}$   
155 thiophene is between 2 and 4 times higher than for DAY.

156 In HY,  $\Delta E_{\text{int}}$  of thiophene is of 90.9 kJ/mol. This adsorption is governed by the interactions of  
157 the protonated sites in HY, with the sulfur atom at a distance of 3.29 Å, and with carbons at  
158 distances of 2.13 to 3.81 Å (Table S1).

159 For LiY, NaY, KY, and CsY,  $\Delta E_{\text{int}}$  of thiophene are of 64.6 kJ/mol, 76.2 kJ/mol, 81.6 kJ/mol,  
160 and 99.2 kJ/mol, respectively. These results indicate a particular behavior where the total



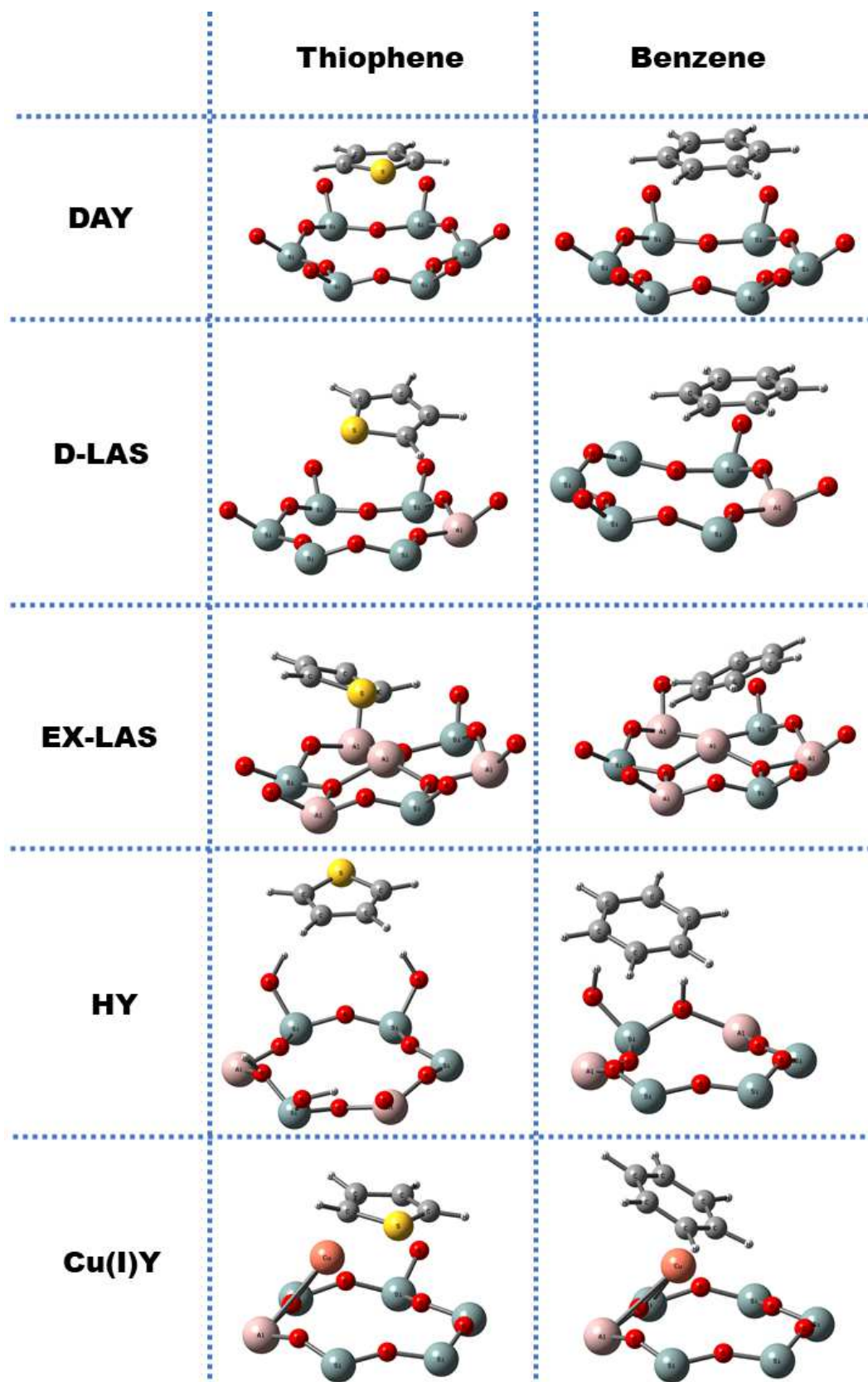
161 interaction energy of thiophene with alkali-FAU increases with the size of the alkali cation.  
162 Moreover, our results are in agreement with Takahashi *et al.* [28] who indicated adsorption  
163 enthalpies of thiophene in H-USY (high Si/Al) and NaY at room temperature of 46 and 82  
164 kJ/mol, respectively. Adsorption configurations show that Li<sup>+</sup>, Na<sup>+</sup>, K<sup>+</sup> and Cs<sup>+</sup> interact with  
165 thiophene via the sulfur atom at distances of 3.38 Å, 3.15 Å, 3.42 Å and 3.79 Å respectively,  
166 and via its carbons at distances of 2.50-3.20 Å, 2.80-3.00 Å, 3.17-3.45 Å, 3.58-3.79 Å,  
167 respectively (Table S1). The exchange of alkali cations with transition metal cations (Cu(I),  
168 Cu(II), Ag(I), or Zn(II)) results in a significant increase in the affinity of thiophene for FAU  
169 zeolites as shown by  $\Delta E_{\text{int}}$  which are of 138.8 kJ/mol for Cu(I), 79.3 kJ/mol for Cu(II)Y,  
170 107.3 for Ag(I)Y, and 123.5 kJ/mol for Zn(II)Y. Our results are in agreement with those  
171 obtained by Oliveira *et al.* [67] which indicated a strong adsorption of thiophene on transition  
172 metals by comparison with the Na<sup>+</sup> cation. In these sorbents, cationic transition metals Cu(I),  
173 Cu(II), Zn(II), and Ag(I) interact with the sulfur atom of thiophene at distances of 3.12 Å,  
174 3.71 Å, 3.29 Å, and 3.33 Å respectively, and with its carbons at distances of 2.01-3.40 Å,  
175 3.02-3.68 Å, 2.27-3.71 Å, and 2.37-3.58 Å, respectively (Table S1).

176 For D-LAS and EX-LAS formulations,  $\Delta E_{\text{int}}$  of thiophene are of 112.1 kJ/mol and 172.9  
177 kJ/mol, respectively. The highest adsorption energy of thiophene is observed with EX-LAS.  
178 Considering D-LAS, its 6MR structure interacts with thiophene via the sulfur atom at a  
179 distance of 3.76 Å, and also via carbons at distances of 2.86-3.85 Å. EX-LAS interacts with  
180 the sulfur atom of thiophene at a distance 3.14 Å and also with its carbons at distances of  
181 2.13-3.87 Å. Moreover, interactions between EX-LAS and thiophene are closer than those  
182 observed between D-LAS and thiophene, showing that thiophene interacts more closely with  
183 EX-LAS than with D-LAS.

184 These results show a strong affinity of thiophene for EX-LAS and Cu(I)Y. Interactions  
185 between thiophene and other zeolite formulations decrease in the following order: ZnY > D-

186 LAS  $\approx$  Ag(I) > CsY  $\approx$  HY. This trend is in good agreement with experimental data reported  
187 by Takahashi et al. [28]. Moreover, other experimental data [67] have shown that thiophene is  
188 more adsorbed on transition metals than on alkali metals.

189



190

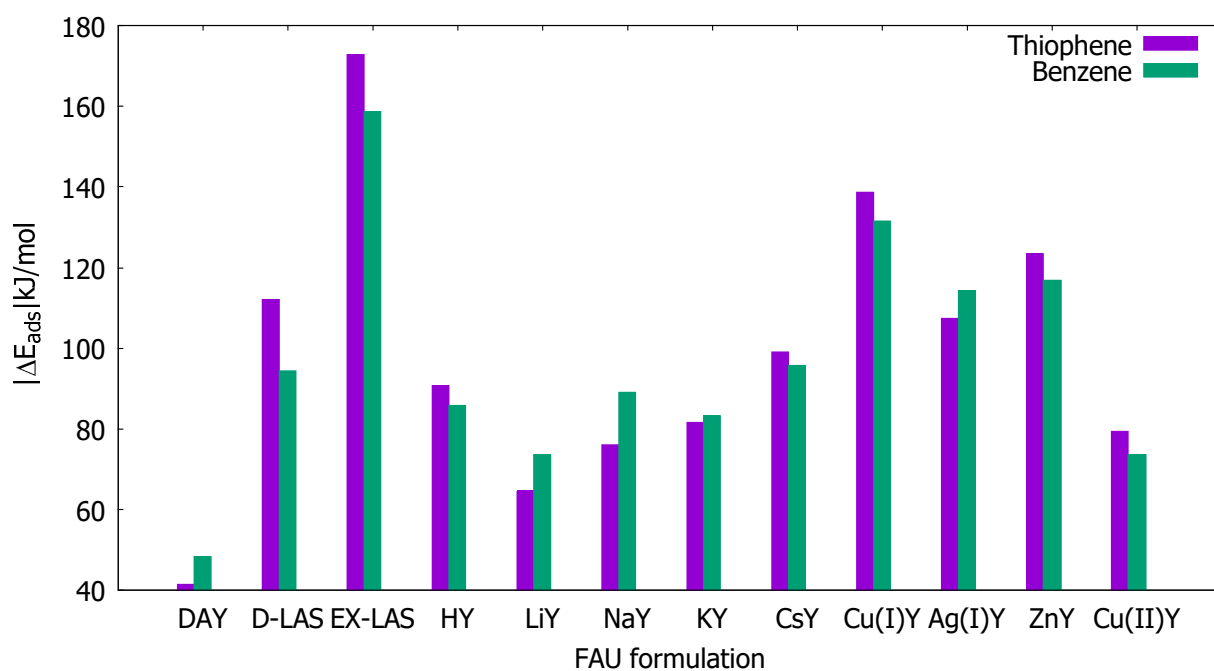
191 **Fig. 1.** Adsorption configurations of thiophene and benzene in DAY, HY, Cu(I)Y, D-LAS,  
 192 and EX-LAS. For the sake of clarity, only the 6MR window surrounding the cation and the  
 193 molecules is displayed. Blue, red, pink, white, gray and yellow balls represent silicon,  
 194 oxygen, aluminum, hydrogen, carbon, and sulfur atoms, respectively.

195

196 **Table 1.** Computed total interaction energies.  $|\Delta E_{\text{int}} \text{ (kJ/mol)}|$  of benzene and thiophene in DAY, MY  
 197 (Si/Al=2.43) and FAU bearing either D-LAS (Si/Al=47) or EX-LAS (Si/Al=15).  
 198

	$ \Delta E_{\text{int}} \text{ (kJ/mol)} $	
	Thiophene	Benzene
<b>DAY</b>	41.5	48.5
<b>D-LAS</b>	112.1	94.4
<b>EX-LAS</b>	172.9	158.6
<b>HY</b>	90.9	85.7
<b>LiY</b>	64.6	73.5
<b>NaY</b>	76.2	89.2
<b>KY</b>	81.6	83.3
<b>CsY</b>	99.2	95.8
<b>Cu(I)Y</b>	138.8	131.4
<b>Ag(I)Y</b>	107.3	114.2
<b>Zn(II)Y</b>	123.5	116.8
<b>Cu(II)Y</b>	79.3	73.6

199



200

201 **Fig. 2.** Total interaction energies of thiophene and benzene molecules, in DAY, D-LAS-  
 202 bearing FAU, EX-LAS-bearing FAU, HY, LiY, NaY, KY, CsY, Cu(I)Y, Ag(I)Y, Zn(II)Y,  
 203 and Cu(II)Y.

204

### 205 3.1.2. Adsorption of benzene

206 In DAY, benzene interacts with the center of a 6MR window via its carbon atoms at distances  
 207 of 3.58-3.93 Å. The total interaction energy calculated for benzene and DAY (48.5 kJ/mol) is

208 the lowest value observed. Indeed, FAU zeolites with any kind of charge compensating cation  
209 or Lewis acid site in their structure exhibit  $\Delta E_{\text{int}}$  with benzene of about 2 to 3 times higher  
210 than for DAY. It is already known that the aromatic components can strongly interact over the  
211 zeolitic acid sites [68–72], as well as the adsorption strength of these molecules  
212 monotonically increases with the cation content [73,74].

213 For HY and NaY, the interaction energies with benzene are 85.7 kJ/mol and 89.2 kJ/mol,  
214 respectively. These values are respectively 37.2 and 40.7 kJ/mol higher than for DAY. For  
215 LiY, KY and CsY,  $\Delta E_{\text{int}}$  with benzene are 73.5, 83.3, and 95.8 kJ/mol, respectively, which are  
216 respectively 25 to 47 kJ/mol higher than for DAY. This trend is consistent with an ONIOM  
217 (Own N-layered Integrated molecular Orbital and molecular Mechanics) study on the  
218 adsorption of benzene in alkali-exchanged FAU and ZSM-5 zeolites [75]. Moreover,  
219 experimental determinations of the adsorption enthalpy of benzene with NaY at room  
220 temperature estimated values of about 76 kJ/mol [76,77]. Since a correction of 10 kJ/mol is  
221 necessary for extrapolating the adsorption energy at 0 K to an adsorption enthalpy at 300 K  
222 [34], our calculations of the total interaction energy at 0K are in good agreement with  
223 experimental results. In HY, we found 2 protons interacting with carbons of the aromatic ring  
224 of benzene at distances of 2.15-3.50 Å (Table S1). However,  $\text{Li}^+$ ,  $\text{Na}^+$ ,  $\text{K}^+$ , and  $\text{Cs}^+$  interact  
225 with carbons of the aromatic ring of benzene at distances of 2.60-2.93 Å, 2.85-2.88 Å, 2.98-  
226 3.39 Å, and 3.59-3.67 Å, respectively (Table S1).

227 For Cu(I)Y and Cu(II)Y,  $\Delta E_{\text{int}}$  with benzene are 131.4 kJ/mol and 73.6 kJ/mol, respectively.  
228 These values are 82.9 kJ/mol and 25.1 kJ/mol higher than for DAY. In these cases, Cu(I) and  
229 Cu(II) cations interact with the carbon atoms of the aromatic ring of benzene respectively at  
230 distances of 2.04-3.23 Å, and 2.98-3.43 Å. Moreover, Cu (I) results in a higher total  
231 interaction energy than Cu (II), showing that the oxidation state of the copper cation has a  
232 clear effect on benzene adsorption in FAU. These results indicate that the interaction of

233 benzene with Cu(I) is more stable than with Cu(II). They are in accordance with Kung studies  
234 [78] which reported that at high oxidation states, metals act as weak Lewis acid sites, resulting  
235 in a weak interaction energy with adsorbed molecules. In addition, using FTIR spectra  
236 Archipov et al. [79] showed that copper undergoes a reduction from Cu(II) to Cu(I) during the  
237 adsorption of benzene.

238 For AgY and Zn(II)Y,  $\Delta E_{\text{int}}$  with benzene are 114.2 kJ/mol and 116.8 kJ/mol, respectively. In  
239 these sorbents, Ag(I) and Zn(II) interact with carbons of the aromatic ring of benzene at  
240 distances of 2.38-3.59 Å and 2.39-3.61 Å, respectively (Table S1). Hence, transition metals  
241 Cu, Ag and Zn show a high total interaction energy with benzene, with Cu exhibiting the  
242 highest one. Again, our theoretical investigations are in agreement with previous experimental  
243 results indicating room temperature adsorption enthalpies of benzene with CuY and AgY of  
244 approximately 91.2 kJ/mol and 84.1 kJ/mol, respectively [28].

245 For D-LAS, the total interaction energy with benzene is 94.4 kJ/mol, which is 45.9 kJ/mol  
246 higher than for DAY. Finally, the highest  $\Delta E_{\text{int}}$  of benzene is observed with EX-LAS (158.6  
247 kJ/mol).

248 Therefore, benzene adsorption with FAU formulations decreased as follows: bearing-EX-LAS  
249 FAU > Cu(I)Y > Zn(II)Y  $\approx$  Ag(I)Y > bearing-D-LAS FAU  $\approx$  CsY > NaY > HY > KY > LiY  
250  $\approx$  Cu(II)Y > DAY. Benzene adsorption in different sorbents is performed through interactions  
251 between charge compensating cations or 6MR (in DAY) and the aromatic cycle of benzene  
252 (Table S1). Our present results are in line with some studies from the literature. Indeed,  
253 Takahashi et al. [28] combined experimental determinations and molecular orbital  
254 calculations for investigating the adsorption of benzene into several sorbents, including Ag-Y,  
255 Cu-Y, Na-Y, and H-USY. Their results showed that benzene highly adsorbs on Cu and Ag  
256 cations through  $\pi$ -complexation. Performing an experimental study, Archipov et al. [79]

257 suggested that benzene adsorption on transition metals is favored by Brønsted sites in Y  
258 zeolite.

259

### 260 *3.2. Selectivity of thiophene adsorption on FAU zeolites in the presence of benzene*

261 The previous results (parts 3.1.1. and 3.1.2.) provided individual details on the adsorption of  
262 thiophene and benzene in various zeolite formulations. Plotting the interaction energies of  
263 benzene and thiophene with the various sorbents (Fig. 2) allows a comparison of the sorbent  
264 affinities for these two molecules.

265 In HY, CsY, Cu(II)Y, Cu(I)Y, and Zn(II)Y, thiophene is slightly more adsorbed than benzene  
266 by 5.2 kJ/mol, 3.4 kJ/mol, 5.7 kJ/mol, 7.4 kJ/mol, 6.7 kJ/mol, respectively. However, in LiY,  
267 NaY, KY, and Ag(I)Y, benzene is slightly more adsorbed than thiophene by 8.9 kJ/mol, 13.0  
268 kJ/mol, 1.7 kJ/mol, and 6.9 kJ/mol, respectively. Such energy differences are too low to  
269 conclude about the sorbent selectivity towards thiophene or benzene. On the other hand,  
270 thiophene is more adsorbed than benzene by 17.7 kJ/mol on D-LAS, suggesting an  
271 outstanding trapping performance for D-LAS towards thiophene. Similarly, EX-LAS could be  
272 a potential candidate for the selective adsorption of thiophene (energy difference of 14.3  
273 kJ/mol). However, its interaction energy with thiophene (172.9 kJ/mol) might be too high to  
274 allow a straightforward regeneration of the sorbent.

275 In general, we can clearly suggest that the two zeolite formulations, D-LAS and EX-LAS,  
276 present a much higher affinity for thiophene than for benzene. They both display Lewis acid  
277 sites. Therefore, we suggest the use of zeolites with a large amount of Lewis acid sites for a  
278 selective trapping of thiophene in presence of benzene. Noteworthy, based on the results of  
279 our current paper, other theoretical approaches could be performed for a limited selection of  
280 formulations to study high coverage such as GCMC and MD simulations, and of course,  
281 dedicated experiments could also be performed.

### 282 3.3. Evaluation of the regenerability of zeolite formulations

283 In addition to the adsorption selectivity criterion, it is also necessary to consider the  
284 possibility of chemical reactions between adsorbed thiophene and the investigated  
285 formulations as well as the formation of by-products, which would reduce the trapping  
286 efficiency and then make the regenerability of the sorbent more difficult [80,81]. To check  
287 this point, we analyzed the length of the two S-C bonds (S-C<sub>1</sub> and S-C<sub>4</sub> as labeled in Fig. 3) in  
288 thiophene in its gaseous phase (before adsorption), and during adsorption over different  
289 formulations. Indeed, three possible situations can arise during adsorption: 1) the first S-C  
290 bond remains as in the gas phase (or decrease a little) and the second is lengthened, 2) both S-  
291 C bonds in thiophene are lengthened, 3) both S-C bonds keep the same distance during  
292 adsorption as in the gas phase. In the first two situations, the elongation of the S-C bond up to  
293 dissociation could result in the molecule destruction, and in completely modifying the degree  
294 of freedom of sulfur atoms. Ultimately, sulfur atoms of thiophene could be released and  
295 precipitate with chemical species present in the adsorption sites. On the other hand, in  
296 situation 1, breaking one S-C bond could allow the capture of the sulfur atom in the  
297 adsorption site, and facilitate breaking of the second S-C bond. In our investigations, analysis  
298 of the bond lengths before and after adsorption showed the following results:

- 299 • In EX-LAS, an elongation of the S-C bond was observed upon adsorption of  
300 thiophene with the order of magnitude of 0.045 Å.
- 301 • In Cu(I)Y, Ag(I)Y, and Zn(II)Y, the S-C bond length was larger upon adsorption than  
302 in the gas phase, by around 0.025Å, 0.016Å, and 0.018Å, respectively.
- 303 • In HY, LiY, NaY, KY, CsY, Cu(II)Y, DAY, and D-LAS, the S-C bond lengths were  
304 roughly similar in the gas phase and upon adsorption.

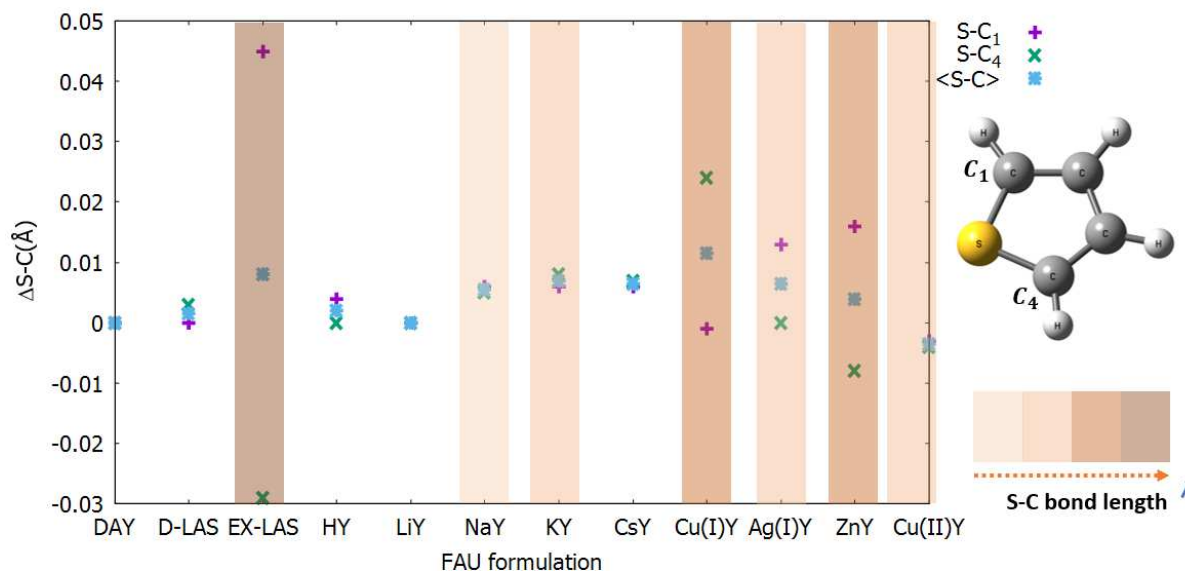
305 Except for EX-LAS, no significant difference was observed in the S-C bond length, between  
306 the gas phase and upon adsorption (no more than 0.03 Å), which ensures that dissociation of



307 thiophene cannot occur after adsorption. This means that in terms of regenerability, all studied  
308 formulations could be safely used for the adsorption of thiophene, except EX-LAS.

309

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311

312 **Fig. 3.** S-C bond length of thiophene in gas phase and upon adsorption.

313

314

#### 315 4. Conclusions

316 In the context of the deep desulfurization of transport fuels, our work aimed at identifying  
317 suitable faujasite (FAU) Y formulations for the selective adsorption of thiophene in the  
318 presence of benzene. Using periodic, vdW-corrected DFT calculations, we systematically  
319 studied the interactions of benzene and thiophene in DAY, FAU containing either Defect  
320 Lewis acid sites (D-LAS) or Extra framework Lewis acid sites (EX-LAS), and MY where M  
321 = H, Li, Na, K, Cs, Cu(I), Cu(II), Ag(I), and Zn(II).

322 Our main results can be summarized as follows:

- 323 (1) Benzene is adsorbed in any FAU formulation through  $\pi$ -interactions, respectively  
324 represented by  $\pi$ -stacking of the aromatic ring on 6MR in DAY, by the interaction of 2

325 protons with the aromatic ring in HY, by M-aromatic ring interactions in MY (M = Li,  
326 Na, K, Cs, Cu(I), Cu(II), Ag(I), and Zn(II)), by Al-aromatic ring interactions in EX-  
327 LAS, and by  $\pi$ -stacking of the aromatic ring on the 6MR containing the negative charge  
328 excess in D-LAS.

329 (2) The affinity of zeolites towards benzene decreases in the following order: bearing-EX-  
330 LAS FAU > Cu(I)Y > Zn(II)Y  $\approx$  Ag (I)Y > bearing-D-LAS FAU  $\approx$  CsY > NaY > HY  
331 > KY > LiY  $\approx$  Cu(II)Y > DAY.

332 (3) Thiophene also adsorbed through its aromatic ring in the various sorbents. However,  
333 the presence of a sulfur atom in its aromatic ring leads to a behavior which is different  
334 from benzene.

335 (4) The affinity of thiophene for zeolites decreases in the following order: EX-LAS >  
336 Cu(I)Y > Zn(II)Y > D-LAS  $\approx$  Ag(I)Y > CsY > HY.

337 Overall, bearing-LAS FAU (D-LAS, and EX-LAS), Cu(I)Y, Cu(II)Y, Zn(II)Y, CsY, and HY  
338 present a higher affinity for thiophene than for benzene. In particular, thiophene is more  
339 adsorbed on D-LAS than benzene by 17.7 kJ/mol, suggesting an outstanding trapping  
340 performance for D-LAS towards thiophene. In terms of regenerability, we have found that all  
341 of the formulations can be used safely except EX-LAS. In conclusion, we recommend the  
342 incorporation of defect Lewis acid sites in Y formulations to obtain a good compromise  
343 between high adsorption selectivity for thiophene in the presence of benzene, and limited C-S  
344 bond activation. Alternatively Zn(II)Y and Cu(II)Y could be tested experimentally for the  
345 ADS technology.

346

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# GRAPHICAL ABSTRACT

